

Air Quality Permitting Technical Memorandum

November 5, 2002

TIER II Operating Permit and Permit to Construct No. 031-00014

McCAIN FOODS INC. BURLEY, IDAHO

Project No. T2-020400

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FINAL PERMIT

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ACRONYMS, UNITS, AND CHEMICAL NOMENCLATURE

AFS AIRS Facility Subsystem

AIRS Aerometric Information Retrieval System

AQCR Air Quality Control Region

ASTM American Society for Testing and Materials

Btu British thermal unit
CO carbon monoxide

Department Department of Environmental Quality
DEQ Department of Environmental Quality
EPA Environmental Protection Agency

IDAPA A numbering designation for all administrative rules in Idaho promulgated in accordance with

the Idaho Administrative Procedures Act

lb/hr pound per hour

MMBtu million British thermal units

NO₂ nitrogen dioxide NO_X nitrogen oxides

NSPS New Source Performance Standards

O₃ ozone

O&M Operation and Maintenance

OP operating permit

PM particulate matter

PM₁₀ particulate matter with an aerodynamic diameter less than or equal to a nominal 10

micrometers

PSD Prevention of Significant Deterioration

PTE Potential to Emit

Rules Rules for the Control of Air Pollution in Idaho

scf standard cubic feet

SIC Standard Industrial Classification

SO₂ sulfur dioxide
SO_x sulfur oxides
T/yr tons per year

VOC volatile organic compound

1. PURPOSE

The purpose for this memorandum is to satisfy the requirements of IDAPA 58.01.01 Sections 200 et seq. and 400 et seq., Rules for the Control of Air Pollution in Idaho.

2. PROJECT DESCRIPTION

This project is for the issuance of a Tier II Operating Permit and Permit to Construct for McCain Foods Inc. located at Burley, Idaho. This permit consolidates all of the emissions sources at the facility into a single permit with federally enforceable conditions that will allow the facility to operate as a synthetic minor source.

3. SUMMARY OF EVENTS

January 21, 2002 DEQ received an application for a Tier II operating permit from McCain Food Inc.

February 19, 2002 The application was declared complete.

June 3, 2002 DEQ issued a facility draft permit for facility review.

August 5, 2002 DEQ issued a proposed permit for public comment.

August 17, 2002 -

September 16, 2002 Public Comment period conducted. No comments were received.

4 FACILITY DESCRIPTION

General Facility Process Description

Prior to processing, trucks deliver raw potatoes from the grower or storage cellars to the site's receiving area. The potatoes are sorted according to size and are temporarily stored in holding bins. Typically, the larger potatoes are transferred to the Prime Products process lines and the smaller potatoes are sent to the Formed Products process lines.

McCain Foods currently operates two process lines for Prime Products, one in each plant. The two plants were originally two facilities, but McCain bought both and they are now combined into one facility in two adjacent areas. McCain's nomenclature refers to the facilities as plant 1 and plant 2. Initially, the potatoes are washed in self-fluming storage bins to remove excess dirt. The potatoes are then conveyed to the peelers. The peelers are pressure vessels in which the potatoes are briefly subjected to high-pressure steam that loosens the skins from the potatoes. The skins are then removed by a scrubber and are transported off-site for use in cattle feed. The potatoes are rinsed in a washer and conveyed to the pretreaters. The pretreaters are warm-water baths that soften the potatoes. The potatoes continue to the trim tables. At the trim tables, potatoes are manually graded and any foreign materials are removed. Low quality potatoes are transported off-site for use in cattle feed.

After being trimmed, the potatoes pass through cutters, which cut them into the desired sizes and shapes. The product is then conveyed over a series of graders to remove any small pieces. These pieces are subsequently diverted to the Formed Products process lines or to cattle feed. The potato products continue to the blanchers. The blanchers are warm-water baths that precondition the potatoes for subsequent processing. The step that follows blanching is called the sugar drag, which is a conditioning and customer quality stage.

Dryers are used to reduce the moisture content of the potato products prior to frying. The two dryers that are operated in conjunction with the Prime Products lines are Prime 1 Dryer (Burley Plant 1) and Prime 2 Dryer (Burley Plant 2). Both of these units are direct-fired dryers that are fueled by natural gas.

After being dried, the potato products are conveyed to fryers where they are cooked in hot vegetable oil. The two fryers that are used for Prime Products are Prime 1 Fryer (Burley Plant 1) and Prime 2 Fryer (Burley Plant 2). The fryers are heated by steam. Each fryer is equipped with an air washer that is essentially a spray-chamber scrubber. In the air washer, exhaust from the fryer is passed through a chamber and contacted with a water spray that saturates the air stream.

The fried products are conveyed into the freezing tunnel. The frozen products are weighed during packaging. On occasion, frozen product will be "cribbed off" or routed to a temporary storage area due to a process problem or for additional quality assurance checks. This product may be added back to the line at the weighing/packaging step at a later time, once all quality issues have been resolved.

Formed Products, such as tater tots and parfries, are manufactured in Burley Plant 1. The Formed Products process is very similar to Prime Products. Smaller potatoes are washed, peeled, and cut. After the potatoes have been cut, they are routed to either the Tot Line or to the Parfry Line.

Potato products in the Tot Line are blanched and conveyed to the Tot Dryer. This unit is a direct, natural gas-fired dryer that removes moisture from the potatoes.

After being dried, the potato products are cut into small slivers and formed into tots. The tots are conveyed to the Tot Fryer in which they are cooked in hot vegetable oil. The fryer is equipped with an air washer that removes PM from the exhaust stream.

The cooked tots are frozen, weighed, and packaged. As in the case of Prime Products, tots may be cribbed off and added back to the line at the weighing/packaging step at a later time.

Potato products in the Parfry Line are blanched and conveyed to the retrograder. The retrograder is not considered an emissions unit because it is a chilling process that is not associated with any combustion sources and does not have external ventilation. The ammonia refrigeration unit associated with the retrograder is a closed-loop system.

After being chilled, to set the starches and allow for easier forming, the potato material is cut into small slivers and formed into parfry patties. The parfry patties are cooked in the Parfry Fryer. The fryer is heated by steam. The cooked parfry patties are frozen, weighed, and packaged. As is the case with Prime Products and tots, parfries may be cribbed off and added back to the line at the weighing/packaging step at a later time.

Four natural gas-fired boilers are used to generate steam for the manufacturing operations at McCain Foods. Two of the units, the Murray 1 Boiler and the Nebraska 1 Boiler, are located in Burley Plant 1. The Murray 1 Boiler has a maximum heat input capacity of 100 MMBtu/hr. The Nebraska 1 Boiler has a maximum heat input capacity of 95.58 MMBtu/hr. The remaining two boilers, the Nebraska 2 Boiler and the Murray 2 Boiler, are located in Burley Plant 2. The Nebraska 2 Boiler has a maximum heat input capacity of 78.05 MMBtu/hr. The Murray 2 Boiler has a maximum heat input capacity of 39.1 MMBtu/hr.

Several of the potato products at McCain Foods are battered. The batter is prepared from various dry ingredients, such as flour and seasonings, in a designated room that is located in Burley Plant 2. Particulate matter is filtered from the air in the batter room by a dust collection system. The system is a package baghouse unit and consists of a group of filter elements that are mounted in an airbox. A diesel fire pump is used at McCain Foods to create water pressure for emergency fire-fighting efforts. The 170 horsepower pump is connected to the Snake River and is located in a small building north of Burley Plant 1. In addition to emergency situations, the emergency fire pump is operated once a week, for approximately two hours, to insure that the unit is functioning properly.

The emissions sources of the facility are:

- (B101) Murray 1 Boiler, Model: MCF4-78, 100 MMBtu/hr
- (B102) Nebraska 1 Boiler, Model: NS-E-68, 95.58 MMBtu/hr
- (B202) Nebraska 2 Boiler, Model: NS-E-57, 78.05 MMBtu/hr
- (B203) Murray 2 Boiler, Model: MCF2-38, 39.1 MMBtu/hr
- (D105 and D106) Prime 1 Dryer, National Model: 59473, 14 MMBtu/hr
- (D107) Tot Dryer, Rey Industries, 4 MMBtu/hr, Direct-Fired Dryer
- (D205–D208) Prime 2 Dryer, National, 48 MMBtu/hr, Direct-Fired Dryer
- (F103) Tot Fryer, Shockey Model: Ore-Ida
- (F104) Prime 1 Fryer, Shockey Model: Ore-Ida
- (F108) Parfry Fryer, Idaho Steel Products Model: Ore-Ida
- (F204) Prime 2 Fryer, Heat and Control
- (E209) Batter Room Collector
- (E001) Emergency Fire Pump, Detroit Diesel Model: 6061-A2

Facility Classification

The facility is a designated facility as defined in IDAPA 58.01.01.006.27 (total maximum rated heat inputs of the boilers at the facility exceeds 250 MMBtu/hr.). The AIRS Facility Subsystem classification is SM because potential emissions of any criteria pollutant are limited to less than 100 tons per year by production limitations. The facility is not subject to PSD permitting requirements for a major modification because the designated facility's PTE is less than 100 T/yr for any criteria pollutant. This facility is a frozen food processor of potato products, SIC code 2037.

Area Classification

McCain Foods Inc., Cassia County, Idaho, is located in AQCR 64. The area is classified as unclassifiable for all federal and state criteria air pollutants (i.e., PM_{10} , SO_x , O_3 , NO_2 , CO, and Pb). (There are no class I areas within 10 km of the facility.)

5. TECHNICAL ANALYSIS

Emissions Estimates

McCain foods provided emissions for the facility using emissions estimated from stack testing and AP-42 values. The emissions in Table 1 are expected if the facility operates at maximum capacity (i.e., at the PTE). Emissions calculations are provided in Appendix A.

Table 4.1. POTENTIAL FACILITY EMISSIONS

Pollutants	Emission Rate				
Pollutaints	lb/hr	Т/ут			
VOCs (as Total Hydrocarbons)	8.98	24.75			
Carbon Monoxide (CO)	51.03	88.22			
Nitrogen Oxides (NO _x)	45,83	72.49			
Particulate Matter (PM ₁₀)	27.44	84.49			
Sulfur Dioxide (SO₂)	0.57	0.42			

Modeling

McCain Foods submitted a facility-wide application to limit potential emissions below major source thresholds at their Burley, Idaho facility. Facility-wide modeling was submitted with the application to demonstrate that emissions from the facility would not cause or significantly contribute to a violation of an ambient air quality standard, as required by IDAPA 58.01.01.403.02.

DEQ has reviewed the analyses and supporting materials submitted, and has verified that operation of the McCain Foods facility as specified in the application will satisfy the requirements of IDAPA 58.01.01.403.02. Review of ambient air impacts of Toxic Air Pollutant emissions indicated that emissions would not unreasonably impact human health, as required by IDAPA 58.01.01.161 and DEQ policy. The Modeling review of McCain Foods Inc. permit application can be found in the Appendix B.

Regulatory Review

1. Scope

This project is for the issuance of a Tier II Operating Permit and Permit to Construct for McCain Foods Inc. located at Burley, Idaho. This permit incorporates all of the emissions sources at the facility into a single permit with federally enforceable conditions that will allow the facility to operate as a synthetic minor source.

2. Facility-wide Conditions

The facility-wide conditions are summarized in the Table 2.

Table 5.1. SUMMARY OF FACILITY-WIDE CONDITIONS

Parameter	Permit Limit / Standard Summary	Applicable Requirements Reference
Fugitive emissions	Reasonable precautions	IDAPA 58.01.01.650-651
Odorous gas, liquids, or solids	No emissions that cause air pollution	IDAPA 58.01.01.775-776
Opacity	20%	IDAPA 58.01.01.625
Excess emissions	In compliance with IDAPA 58.01.01.130-136	IDAPA 58.01.01.130
Open burning	In accordance with IDAPA 58.01.01.600-616	IDAPA 58.01.01.600-616
PM ₁₀ , PM, NO _x , SO ₂ , CO, VOC, Opacity	Test methods	IDAPA 58.01.01.157
Fuel-burning equipment PM Standard	Grain loading	IDAPA 58.01.01,676-677
Fuel oil sulfur content	ASTM grade 1 - 0.3 % ASTM grade 2 - 0.5 %	IDAPA 58.01.01.728
Air Stagnation Advisory Days	Comply with Air Pollution Emergency Rules in IDAPA 58.01.01.550-562	IDAPA 58.01.01.550-562

3. Boilers

Emissions Limit - (Permit Condition 3.3)

Emissions are limited in Permit Condition 3.3 to the levels listed in Table A1 in the permit to make the facility a synthetic minor. The boilers are limited to total emissions from the combination of all boilers in use at any time. This allows McCain Foods to operate the boilers in the configuration most practical for whatever product is being produced at that time. The emissions estimate for the facility was determined from a compilation of AP-42 emissions factors and source testing. The emissions calculations can be found in Appendix A.

Compliance Demonstration

Fuel Usage Limits

The collective natural gas consumption by the boilers shall not exceed 1,100 MMscf/yr for any consecutive 12-month period.

Fuel Meter

Within 90 days of the issuance of the permit, the permittee shall install, calibrate, maintain, and operate a natural gas flow meter to monitor the monthly and annual natural gas usage of the boilers.

Fuel Type

All the boilers shall be fueled on natural gas exclusively. The maximum total rated heat input capacity is 313 MMBtu per hour.

Monitor Operating Parameters

The permittee shall record the following parameters in a log to demonstrate compliance with the natural gas usage requirements for the boilers at the facility:

- Calendar date and total amount of natural gas burned, in standard cubic feet per month or therms per month, by the four boilers, collectively.
- Calendar date and amount of natural gas burned, in standard cubic feet per year or therms
 per year for any consecutive 12-month period, by the four boilers, collectively.

NSPS Applicability

The requirements of 40 CFR 60, Subpart D is not applicable for these boilers because all the boilers were installed prior to June 9, 1989.

4. Dryers

Emissions Limit - (Permit Condition 4.3)

Emissions are limited in Permit Condition 4.3 to the levels listed in Table A1 in the permit to make the facility a synthetic minor. The emissions estimate for the facility was determined from a compilation of AP-42 emissions factors and source testing. The emissions calculations can be found in Appendix A.

Compliance Demonstration

Throughput Limits

The maximum throughput of the Prime 1 Dryer shall not exceed 642 tons/day of finished potato product. The maximum annual throughput of the Prime 1 Dryer shall not exceed 173,340 tons of finished potato product per any consecutive 12-month period.

The maximum throughput of the Prime 2 Dryer shall not exceed 540 tons/day of finished potato product. The maximum annual throughput of the Prime 2 Dryer shall not exceed 145,800 tons of finished potato product per any consecutive 12-month period.

The maximum throughput of the Tot Dryer shall not exceed 192 tons/day of finished potato product. The maximum annual throughput of the Tot Dryer shall not exceed 51,840 tons of finished potato product per any consecutive 12-month period.

Fuel Usage Limits

The maximum combustion of natural gas in the Tot Dryer shall not exceed 30 MMscf/yr for any consecutive 12-month period.

The maximum combustion of natural gas in the Prime 1 Dryer shall not exceed 75 MMscf/yr for any consecutive 12-month period.

The maximum combustion of natural gas in the Prime 2 Dryer shall not exceed 120 MMscf/yr for any consecutive 12-month period.

Fuel Meter

Within 90 days of the issuance of the permit, the permittee shall install, calibrate, maintain, and operate a natural gas flow meter to monitor the monthly and annual natural gas usage for the Prime 1 Dryer, Prime 2 Dryer, and Tot Dryer.

Fuel Type

The dryers shall be fueled on natural gas exclusively.

Throughput Monitoring

Each month, the permittee shall monitor and record the throughput of Prime 1 Dryer, Prime 2 Dryer, and Tot Dryer for that month and for the most recent 12-month period. The throughput shall be measured at the packaging step of each process line and shall take into account product that has been manufactured during a 24-hour period.

Monitor Operating Parameters

The permittee shall record the following parameters in a log to demonstrate compliance with the natural gas usage requirements for the Prime 1 Dryer, Prime 2 Dryer, and Tot Dryer at the facility:

 Calendar date and total amount of natural gas burned, in standard cubic feet per month or therms per month, by the Prime 1 Dryer, Prime 2 Dryer, and Tot Dryer. Calendar date and amount of natural gas burned, in standard cubic feet per year or therms per yr for any consecutive 12-month period, by the Prime 1 Dryer, Prime 2 Dryer, and Tot Dryer.

Fryers

Emissions Limit - (Permit Condition 5.3)

Emissions are limited in Permit Condition 5.3 to the levels listed in Table A1 in the permit to make the facility a synthetic minor. The emissions estimate for the facility was determined from a compilation of AP-42 emissions factors and source testing. The emissions calculations can be found in Appendix A.

Compliance Demonstration

Throughput Limits

The maximum throughput of finished potato product for the Prime 1 Fryer shall not exceed 642 tons/day based on a 24-hour average or 173,340 T/yr for any consecutive 12-month period.

The maximum throughput of finished potato product for the Prime 2 Fryer shall not exceed 540 tons/day based on a 24-hour average or 145,800 T/yr for any consecutive 12-month period.

The maximum throughput of finished potato product for the Tot Fryer shall not exceed 192 tons/day based on a 24-hour average or 51,840 T/yr for any consecutive 12-month period.

The maximum throughput of finished potato product for the Parfry Fryer shall not exceed 61.2 tons/day based on a 24-hour average, or 16,524 T/yr for any consecutive 12-month period.

Air Pollution Control Equipment

The fan and the spray-water pump associated with each air washer shall be operated per the instructions provided in the O&M manual. The pressure at the header of the air washer shall also be set per the specifications identified in the O&M manual by adjusting the pump discharge valve.

The air washer system shall be maintained on a routine basis in accordance with the schedule recommended in the O&M manual. Maintenance activities shall include, but not be limited to, the following:

- Cleaning and replacing the spray-water nozzles,
- · Maintaining the pressure pump, and
- · Cleaning the eliminator blades.

Throughput Monitoring

Each month, the permittee shall monitor and record the throughput of Prime 1 Fryer, Prime 2 Fryer, Tot Fryer, and Parfry Fryer for that month and for the most recent 12-month period. The throughput shall be measured at the packaging step of each process line and shall take into account product that has been manufactured during a 24-hour period.

Air Pollution Control Parameters

The permittee shall monitor and record the parameters listed below to demonstrate compliance with air pollution control equipment requirements for Prime 1 Fryer Air Washer, Prime 2 Fryer Air Washer, Tot Fryer Air Washer, and Parfry Fryer Air Washer.

- · Air washer fan is operable. Verify once daily and record status in log.
- · Spray-water pump is operable. Verify once daily and record status in log.
- · Spray-water pump pressure. Measure once daily and record pressure in log.
- · Maintenance activities. Record date and description in log.

Operations and Maintenance Manual

Within 180 days of issuance of this permit, the permittee shall have developed an O&M manual for the fryer air washers (air pollution control devices). The O&M manual shall describe the procedures that will be followed to insure proper operation of the fryer air washers. The manual shall remain onsite at all times.

6. Batter Room

Emissions Limit - (Permit Condition 6.3)

Émissions are limited in Permit Condition 6.3 to the levels listed in Table A1 in the permit to make the facility a synthetic minor. The emissions estimate for the facility was determined from a compilation of AP-42 emissions factors and source testing. The emissions calculations can be found in Appendix A.

Compliance Demonstration

Baghouse Pressure Drop

The pressure drop across the baghouse shall be maintained within manufacturer's specifications. Documentation of the operating pressure drop specifications for the baghouse shall remain onsite at all times.

Baghouse Operation Monitoring

The permittee shall inspect the Batter Room Dust Collector filters once per month, for tears and holes. The filters shall be replaced as needed. The filter status shall be recorded in a log.

7. Emergency Fire Pump

Emissions Limit – (Permit Condition 7.3)

Emissions are limited in Permit Condition 7.3 to the levels listed in Table A1 in the permit to make the facility a synthetic minor. The emissions estimate for the facility was determined from a compilation of AP-42 emissions factors and source testing. The emissions calculations can be found in Appendix A. The emergency fire pump is not subject the grainloading standards set forth in IDAPA 58.01.01.676-677, this standard is for fuel burning equipment and not internal combustion engines.

Compliance Demonstration

Hours of Operation

The maximum hours of operation for the Emergency Fire Pump shall not exceed two hours per week, except during an emergency. The total number of hours of operation for the Emergency Fire Pump shall not exceed 104 hours for any consecutive 12-month period.

Fuel Specification

The Emergency Fire Pump shall be fired exclusively by No. 2 diesel fuel. The sulfur content of the No. 2 diesel fuel shall be less than 0.5% by weight.

Operation Monitoring

The permittee shall monitor and record the date and the number of hours of operation of the Emergency Fire Pump to verify compliance with the operating parameters previously stated.

8. Emissions Inventory

Table 5.2 ALLOWABLE EMISSIONS

McCain Foods, Burley Emission Estimates* – Hourly (lb/hr) and Annual ^b (T/yr)												
		Annual PM ₁₀ °	NO _x		co		VOC		SO₂			
Source Description	Emissions (lb/hr)	Emissions (T/yr)	lb/hr	T/yr	lb/hr	T/yr	lb/hr	T/yr	lb/hr	Tlyr		
(B101) Murray 1 Boiler	0.75		9.80		8.24		0.54		0.06			
(B102) Nebraska 1 Boiler	0.71	4.18	9.37		7.87	46.20	0.52	3.03	0.02	0.33		
(B202) Nebraska 2 Boiler	0.58	4.10	7.65		6.43	40.20	0.42		0.06			
(B203) Murray 2 Boiler	0.29		3.83		3.22		0.26		0.05			
(D105 and D106) Prime 1 Dryer	6.69	21.67	2.10	5.74	5.12	13.99	0.08	0.21	0.01	0.02		
(D107) Tot Dryer	2.00	6.48	0.60	2.30	1.46	5.60	0.02	80.0	0.002	0.01		
(D205-D208) Prime 2 Dryer	5.63	18.23	7.20	9.18	17.55	22.38	0.26	0.33	0.03	0.04		
(F103) Tot Fryer	4.08	13.22					1.20	3.89				
(F104) Prime 1 Fryer	2.68	8.67					2.68	8.67				
(F108) Parfry	1.30	4.21		++			0.38	1.24		ш-		
(F204) Prime 2 Fryer	2.25	7.29					2.25	7.29		44.		
(E209) Batter Room Collector	0.12	0.53	- -		4 -			wa.	+			
(E001) Emergency Fire Pump	0.37	0.02	5.27	0.27	1.14	0.06	0.43	0.02	0.35	0.02		

^{*} As determined by a pollutant-specific U.S. EPA reference method, a Department-approved alternative, or as determined by the Department's emissions estimation methods used in this permit analysis.

* As determined by multiplying the actual or alternative (for a standard by multiplying the actual or alternative).

^b As determined by multiplying the actual or allowable (if actual is not available) pound per hour emission rate by the allowable hours per year that the process(es) may operate(s), or by actual annual production rates.

c includes condensables.

9. Airs

AIRS/AFS' FACILITY-WIDE CLASSIFICATION' DATA ENTRY FORM

AIR PROGRAM	SIP ¢	PSD 4	NSPS.	NESHAP!	MACT ⁸	TITLE	AREA CLASSIFICATION A – Attainment
POLLUTANT	Sir	Pau	(Part 60)	(Part 61)	(Part 63)	V	U – Unclassifiable N – Nonattainment
SO₂ [†]	В						U
NO, '	SM		·			5M	U
CO ₁	SM					5m	U
PM ₁₀ *	SM					SM	U
PT (Particulate) ¹	SM					SM	U
VOC *	B						U
THAP (Total HAPs) "	В						U
			APP	LICABLE SUB	PART		

- Aerometric Information Retrieval System (AIRS) Facility Subsystem (AFS)
- b AIRS/AFS Classification Codes:
 - A = Actual or potential emissions of a pollutant are above the applicable major source threshold. For NESHAP only, class "A" is applied to each pollutant which is below the 10 T/yr threshold, but which contributes to a plant total in excess of 25 T/yr of all NESHAP pollutants.
 - SM = Potential emissions fall below applicable major source thresholds if and only if the source complies with federally enforceable regulations or limitations.
 - B = Actual and potential emissions below all applicable major source thresholds.
 - C = Class is unknown.
 - ND = Major source thresholds are not defined (e.g., radionuclides).
- State Implementation Plan
- ^d Prevention of Significant Deterioration
- New Source Performance Standards
- National Emission Standards for Hazardous Air Pollutants
- Maximum Achievable Control Technology
- Sulfur Dioxide
- Nitrogen Oxides
- Carbon Monoxide
- * Particulate matter with an aerodynamic diameter less than or equal to a nominal 10 micrometers
- Particulate Matter
- Wolatile Organic Compounds
- " Hazardous Air Pollutants

6. FEES

The facility is current with Tier I registration fees in accordance with IDAPA 58.01.01.387. The facility is not required to pay the Tier II processing fee per IDAPA 58.01.01.407.02.d.

7. RECOMMENDATIONS

Based on the review of the application materials, and all applicable state and federal regulations, staff recommends that DEQ issue a Tier II Operating Permit and Permit to Construct to McCain Foods Inc. An opportunity for public comment on the air quality aspects of the proposed permit has been provided in accordance with IDAPA 58.01.01.404.01.c.

SC/wg/sm G:\AIR QUALITY\STATIONARY SOURCE\SS LTD\T2\MCCAIN FOODS\FINAL PERMIT\T2-020400 FINAL T M.DOC

APPENDIX A Emission Calculations

Air Pollutant Emissions Burley Plant 1 - Tot Dryer (D107)

Combustion Source Charac	teristics	Stack Data ^c	
Manufacturer	Rey Industries	Proposed Stack Height (ft)	52.5
Model	None	Stack Diameter (ft)	2.99
Input Heat Capacity (BTU/hr)	4,000,000	Exit Gas Temperature (°F)	118.1
Fuel	Natural Gas	Exit Gas Moisture Content	4.62%
Heating Value (BTU/scf)	1,020	Wet Actual Flow Rate (acfm)	19,173
Max Hourty Fuel Consumption (scf/hr)	3,922	Wet Standard Flow Rate (wscfm)	15,297
Annual Fuel Consumption (scflyr)*	30,000,000	Dry Standard Flow Rate (dscfm)	14,590
Pariotal Por Community and Community		Stack Gas Velocity (m/s)	13,92
Process Characteristi	CS	Stack Gas Pressure (mm Hg)	663.96
Max Hourly Production Rate (lb/hr)	16,000	•	
Annual Production Rate (TPY)*	51,840		

teris Pollut Pollutant	Poliulant Source	Emission Factor ^a	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)	Significant Level* (TPY)	Below Regulatory Concern? ⁱ	Significant Contribution?
PM ₁₀	NG Combustion & Process	See PM	See PM	2.000	6.480	0.252	15	no	no
SO ₂	NG Combustion	0.6	lb/10 ⁸ scf	0.002	0.009	2.96E-04	40	y e #	no
NO,	NG Combustion & Process	153	lb/10 ⁶ scf	0.600	2.295	0.076	40	yes	ne
co	NG Combustion & Process	373	lb/10 ⁶ scf	1.463	5.595	0.184	100	yes	no
voc	NG Combustion	5.5	lb/10 ⁸ scf	0.022	0.083	0.003	40	y es	no
Lead	NG Combustion	0.0005	lb/10 ⁶ scf	1.96E-06	7,50E-06	2.47E-07	0.6	yes	no

Non-Criteria Pollutants with Significant Threshold										
		Emission	Emission	Potential Emissions			Significant Level*	Below Regulatory	Significant	
Pollutant	Pollutant Source	Factor ^d	Factor Unit	(lb/hr)	(TPY)	(g/s)	(TPY)	Concern?	Contribution?*	
PM	NG Combustion & Process	0.25	lb/finished ton	2.000	6.480	0.252	25	no	no	
Beryffium	NG Combustion	<1.2E-5	lb/10 ^e scl	4.71E-08	1.80E-07	5.93E-09	0.0004	yes	nó	
Mercury	NG Combustion	2.60E-04	lb/10 ⁶ scf	1.02E-06	3.90E-06	1.28E-07	0.1	yes	no	

Other Pollutants									
Pollutent	Poliutani Source	Emission Factor ^d	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (0/s)			
тос	NG Combustion	11	Ib/10 ⁶ scf	0.043	0.165	0.005			
Methane	NG Combustion	2.3	lb/10 ⁶ scf	0.009	0.035	0.001			
CO,	NG Combustion	120,000	lb/10° scf	471	1800	59.3			
N ₂ O	NG Combustion	2.2	lb/10 ⁸ scf	0.000	0.033	0.001 -			

Process Weight Rule®									
Pollutant	Poliutant Source	Potential Emissions (lb/hr)	Potential Emissions (gr/dscf)	Allowable Emissions (or/dscf)	Meets Standard?				
PM	Process	2.000	0.016	0.2	yes				

PM Grain Loading Standard - Not Applicable

- (a) The annual natural gas consumption for this emission unit will be limited.
- (b) The annual production rate associated with this emission unit will be limited. Estimate is equivalent to operating 300 days per year at 90% of maximum hourly production rate.
- (c) Stack gas flow data obtained from testing conducted in November 2001.
- (d) Emission factors for NO, and CO generated by the process and natural gas combustion based on April 1994 Ore-Ida Source Test (Ontario, OR - Prime 1 North Dryer). Emission factors for PM generated by the process and natural gas combustion based on October 1994 Ore-Ida Source Test (Burley, ID - Prime 1 Dryer), April 1995 Ore-Ida Source Test (Ontario, OR - P1 Dryer) and February 1997 Ore-Ida Source test (Ontario, OR - P2 & P3 Dryers). As a conservative approach, emissions that were measured as PM during the source tests were considered to equal PM₁₀. Emission factors for other pollutants from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (e) IDAPA 58.01.01.006.92
- (f) IDAPA 58.01.01.221.01
- (g) IDAPA 58.01.01.710.08. Process weight rule standard is 0.2 gr/dscf for units constructed or modified prior to July 1, 2000.

Toxic Air Pollutant Emissions Burley Plant 1 - Tot Dryer (D107)

Stack Datas

52.5

2.99

118.1

4.62%

19,173

15,297

14,590

13.92

663.96

Combustion Source Characteristics Proposed Stack Height (ft) Rey Industries mer Manufacturer Stack Diameter (ft) None del 4,000,000 Exit Gas Temperature (°F) ut Heat Capacity (BTU/hr) **Exit Gas Moisture Content** Natural Gas 1,020 Wet Actual Flow Rate (acfm) ating Value (BTU/scf) Wet Standard Flow Rate (wscfm) x Hourly Fuel Consumption (scf/hr) 3,922 30,000,000 Dry Standard Flow Rate (dscfm) nual Fuel Consumption (scf/yr)* Stack Velocity (m/s) Stack Gas Pressure (mm Hg)

Process Characteristics x Hourly Production Rate (lb/hr) 16,000

nual Production Rate (TPY)

51,840

Air Poliutants		Emission	Potential Emissions	Potential Emissions	Potential Emissions	Emission Limit	Modeling
Pollutant	Emission Factor ^d	Factor Unit	(lb/hr)	(TPY)	(9/8)	(ID/hr)	Required?
Arsenic	2.00E-04	lb/10 ⁶ scf	7,84E-07	3.00E-06	9.88E-08	1.50E-06	no
Barium	4,40E-03	/b/10 ⁶ scf	1.73E-05	6.60E-05	2.17E-06	3.30E-02	no
Benzene	2.10E-03	lb/10 ⁶ scf	8.24E-06	3.15E-05	1.04E-06	8,00E-04	no
Beryllium	<1.2E-5	lb/10 ⁶ scf	4.71E-08	1.80E-07	5.93E-09	2.80E-05	no
Benzo(a)pyrene	<1.2E-6	lb/10 ⁶ scf	4.71E-09	1.80E-08	5.93E-10	2.00E-06	no
is (2-ethythexyl)phthalate	FNA	lb/10 ⁶ scf	FNA	FNA	FNA	2.80E-02	no
Cadmium	1.10E-03	lb/10 ⁶ scf	4.31E-06	1.65E-05	5.44E-07	3.70E-06	y + \$
Chromium	1.40E-03	lb/10 ⁶ scf	5.49E-06	2.10E-05	6.92E-07	3.30E-02	no
Cobell	8.40E-05	lb/10 ⁸ scf	3.29E-07	1.26E-06	4.15E-08	3.30E-03	no_
Соррег	8.50E-04	lb/10 ⁶ scf	3.33E-06	1,28E-05	4.20E-07	3,33E-01	no
Dibutylphthalete	FNA	1b/10 ⁶ scf	FNA	FNA	FNA	6.70E-02	no
Dichlorobenzene	1.20E-03	lb/10 ⁶ scf	4.71E-06	1.80E-05	5.93E-07	2.00E+01	no
Ethylbenzene	FNA	lb/10 ⁶ scf	FNA	FNA	FNA	2.90E+01	no
Fluorene	2.80E-06	lb/10 ⁶ scf	1.10E-08	4.20E-08	1.38E-09	1,33E-01	no
Formaldehyde	7.50E-02	lb/10 ⁶ scf	2.94E-04	1.13E-03	3.71E-05	5.10E-04	no
Hexane	1.80E+00	lb/10 ⁶ scf	7.06E-03	2.70E-02	8.89E-04	1.20E+01	no
Manganese	3.80E-04	lb/10 ⁶ scf	1,49E-06	5.70E-06	1.88E-07	3.33E-01	no
Mercury	2.60E-04	lb/10 ⁸ scf	1.02E-06	3.90E-06	1.28E-07	3.00E-03	no
Molybdenum	1.10E-03	lb/10 ⁶ scf	4.31E-06	1.65E-05	5.44E-07	3.33E-01	no
Napthalene	6.10E-04	lb/10 ⁶ scf	2.39E-06	9.15E-06	3.01E-07	3.33E+00	no
Nickel	2.10E-03	lb/10 ⁶ scf	8.24E-06	3.15E-05	1.04E-06	2.70E-05	no
Pen tane	2.60E+00	lb/10 ⁶ scf	1.02E-02	3.90E-02	1.28E-03	1.18E+02	no
Phenol	FNA	lb/10 ⁸ scf	FNA	FNA	FNA	1.27E+00	no
Selenium	<2.4E-5	lb/10 ⁶ scf	9.41E-08	3.60E-07	1.19E-08	1.30E-02	no
Toluene	3.40E-03	lb/10 ⁶ scf	1.33E-05	5.10E-05	1.68E-06	2.50E+01	no
Vanadium	2.30E-03	lb/10 ⁶ scf	9.02E-06	3,45E-05	1,14E-06	3.00E-03	no
o-Xylene	FNA .	lb/10 ⁶ scf	FNA	FNA	FNA	2.90E+01	** ***********************************
Zinc	2.90E-02	lb/10 ⁶ scf	1,14E-04	4.35E-04	1,43E-05	6.67E-01	no

98:

The annual natural gas consumption for this emission unit will be limited.

The annual production rate associated with this emission unit will be limited. Estimate

s equivalent to operating 300 days per year at 90% of maximum hourly production rate.

stack gas flow data obtained from testing conducted in November 2001.

Emission Factors from AP-42 Chapter 1.4, "Natural Gas Combustion".

DAPA 58.01.01.585 and 586

)APA 58.01.01.210.05(b)

'NA - Factor Not Available

Air Pollutant Emissions Burley Plant 1 - Prime 1 Dryer (D105 - D106)

Combustion Source Charac	teristics	Stack D	ata ^c · ·	
Manufacturer	Nebraska	Proposed Stack Height (ft)	60.7	60.7
Model	59473	Stack Diameter (ft)	3.39	3.39
Input Heat Capacity (BTU/hr)	14,000,000	Exit Gas Temperature (°F)	215.8	160.0
Fuel	Natural Gas	Exit Gas Moisture Content	6.68%	5.81%
Heating Value (BTU/scf)	1,020	Wet Actual Flow Rate (actm)	16,417	14,504
Max Hourly Fuel Consumption (sc//hr)	13,725	Wet Standard Flow Rate (wscfm)	11,177	10,741
Annual Fuel Consumption (scf/yr)*	75,000,000	Dry Standard Flow Rate (dscfm)	10,430	10,117
WE HINDS! FOR COMPONING		Stack Velocity (m/s)	9,27	8.19
Process Characterist	cs	Stack Gas Pressure (mm Hg)	662.18	660.91
Max Hourly Production Rate (lb/hr)	53,500		East Stack	West Stack
Annual Production Rate (TPY) ^b	173,340			

iteria Pollut Pollutant	Poliutant Source	Emission Factor ⁶	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)	Significant Level* (TPY)	Below Regulatory Concern?	Significant Contribution?
PM ₁₀	NG Combustion & Process	See PM	See PM	6.688	21.668	0.843	15	по	yes.
SO ₂	NG Combustion	0.6	lb/10 ⁸ scf	0.008	0.023	0.001	40	yes	no
NO,	NG Combustion & Process	153	lb/10 ⁶ scf	2.100	5,738	0.265	40	no	no
CO	NG Combustion & Process	373	lb/10 ⁶ scf	5.120	13,988	0.645	100	no	no
VOC	NG Combustion	5.5	lb/10 ⁶ scf	0.075	0.206	0.010	40	yes	no
Lead	NG Combustion	0.0005	lb/10 ⁶ scf	6.86E-06	1.88E-05	8.65E-07	0.6	yes	. ue

Non-Criteria Po	llutants with Signifi	cant Thresho	old		-			11.1	
		Emission	Emission	Potential Emissions	Potential Emissions	Potential Emissions		Below Regulatory	Significant
Pollutant	Pollutant Source	Factor 6	Factor Unit	(lb/hr)	(TPY)	(9/8)	(TPY)	Concern?	Contribution?*
PM	NG Combustion & Process	0.25	lb/finished ton	6.688	21,668	0.843	25	no	no ·
Beryllium	NG Combustion	<1.2E-5	lb/10 ⁵ scf	1.65E-07	4.50E-07	2.08E-08	0.0004	yes.	no
Mercury	NG Combustion	2.60E-04	lb/10 ⁶ scf	3.57E-06	9.75E-06	4.50E-07	0.1	yes	no

Pollulant	Pollutant Source	Emission Factor ⁶	Emission Fector Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
TOC	NG Combustion	11	lb/10 ⁸ scf	0.151	0,413	0.019
Methane	NG Combustion	2.3	lb/10 ⁶ scf	0.032	0,086	0.004
CO ₂	NG Combustion	120,000	lb/10 ⁶ scf	1647	4500	207.5
N ₂ O	NG Combustion	2,2	lb/10 ⁶ scf	0.030	0.083	0.004

Process Weight	Rule [®]					
		Potential	E. Stack	W. Stack	Allowable	Ali Stacks
		Emissions	Emissions	Emissions	Emissions	Meet
Poliutant	Pollutani Source	(lb/hr)	(gr/dscf)	(gr/dscf)	(gr/dscf)	Standard?
PM	Process	6.688	0.075	0.077	0.2	yes

PM Grain Loading Standard - Not Applicable

- (a) The annual natural gas consumption for this emission unit will be limited.
- (b) The annual production rate associated with this emission unit will be limited. Estimate is equivalent to operating 300 days per year at 90% of maximum hourly production rate.
- (c) This emission unit vents to the atmosphere via two stacks. Stack gas flow data obtained from testing conducted in November 2001.
- (d) Emission factors for NO, and CO generated by the process and natural gas combustion based on April 1994 Ore-Ida Source Test (Ontario, OR - Prime 1 North Dryer). Emission factors for PM generated by the process and natural gas combustion based on October 1994 Ore-Ida Source Test (Burley, ID - Prime 1 Dryer), April 1995 Ore-Ida Source Test (Ontario, OR - P1 Dryer) and February 1997 Ore-Ida Source test (Ontario, OR - P2 & P3 Dryers). As a conservative approach, emissions that were measured as PM during the source tests were considered to equal PM₁₀. Emission factors for other pollutants from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (e) IDAPA 58.01.01.006.92
- (f) IDAPA 58.01.01.221.01
- (g) IDAPA 58.01.01.710.08. Process weight rule standard is 0.2 gr/dscf for units constructed or modified prior to July 1, 2000.
- (h) IDAPA 58.01.01.676 or 677 The Prime 1 Dryer is a direct heat transfer system. Therefore, it does not satisfy the definition of "fuel burning equipment" as presented in IDAPA 58.01.01.006.41.
- * NA Not Applicable

Toxic Air Pollutant Emissions Burley Plant 1 - Prime 1 Dryer (D105 - D106)

Combustion Source Cha	racteristi cs	Stack Date	B _C	
	Nebraska	Proposed Stack Height (ft)	60.7	60.7
THE	59473	Stack Diameter (ft)	3.39	3.39
del ut Heat Capacity (BTU/hr)	14,000,000	Exit Gas Temperature (*F)	215.8	160.0
al de la Capacity (D Com)	Natural Gas	Exit Gas Moisture Content	6.68%	5.81%
ating Value (BTU/scf)	1,020	Wet Actual Flow Rate (acfm)	16,417	14,504
x Hourly Fuel Consumption (scf/hr)	13,725	Wet Standard Flow Rate (wscfm)	11,177	10.741
nual Fuel Consumption (scl/yr)*	75,000,000	Dry Standard Flow Rate (dscfm)	10,430	10,117
ilder Faci Consumption (1-1-7)	•	Stack Velocity (m/s)	9.27	8.19
Process Characteri	stics ·	Stack Gas Pressure (mm Hg)	662.18	660.91
x Hourly Production Rate (lb/hr)	53,500		East Stack	West Stack
nual Production Rate (TPY) ^b	173,340			

Air Pollutants Pollutant	Emission Factor *	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)	Emission Limit* (lb/hr)	Modeling Required
Arsenic	2.00E-04	lb/10 ⁶ scf	2.75E-06	7.50E-06	3,46E-07	1.50E-06	y e \$
Berium	4.40E-03	lb/10 ⁸ scf	6.04E-05	1.65E-04	7.61E-06	3.30E-02	no
Benz ene	2.10E-03	lb/10 ^c scf	2.88E-05	7.88E-05	3,63E-06	8,00E-04	ΠÖ
Beryllium	<1.2E-5	lb/10 ⁶ scf	1.65E-07	4.50E-07	2.08E-08	2.80E-05	no
Benzo(a)pyrene	<1.2E-6	lb/10 ⁶ scf	1.65E-08	4.50E-08	2.08E-09	2.00E-06	no
is (2-ethylhexyl)phthalate	FNA	lb/10 ⁸ scf	FNA	FNA	FNA	2.80E-02	no
Cadmium	1.10E-03	lb/10 ⁶ scf	1.51E-05	4,13E-05	1,90E-06	3.70E-06	yes
Chromlum	1.40E-03	lb/10 ⁶ scf	1.92E-05	5.25E-05	2.42E-06	3.30E-02	no
Cobalt	8.40E-05	lb/10 ⁸ scf	1.15E-06	3.15E-06	1.45E-07	3.30E-03	no
Copper	8.50E-04	lb/10 ⁶ scf	1.17E+05	3.19E-05	1.47E-06	3.33E-01	no
Dibutylphthalate	FNA	lb/10 ⁶ scf	FNA	FNA	FNA	6.70E-02	no
Dichlorobenzene	1,20E-03	lb/10 ⁶ scf	1,65E-05	4.50E-05	2.08E-06	2.00E+01	no
Ethylbenzene	FNA	lb/10 ⁸ scf	FNA	FNA	FNA	2.90E+01	no
Fluorene	2.80E-06	lb/10 ⁸ scf	3.84E-08	1.05E-07	4.84E-09	1.33E-01	no
Formaldehyde	7.50E-02	lb/10 ⁶ scf	1.03E-03	2.81E-03	1.30E-04	5.10E-04	yes
Hexane	1.80E+00	lb/10 ⁶ scf	2.47E-02	6.75E-02	3.11E-03	1.20E+01	no
Manganese	3.80E-04	lb/10 ⁶ scf	5,22E-06	1.43E-05	6.57E-07	3.33E-01	no
Mercury	2.60E-04	lb/10 ⁶ scf	3.57E-06	9.75E-06	4.50E-07	3.00E-03	no
Molybdenum	1.10E-03	lb/10 ⁶ scf	1.51E-05	4.13E-05	1.90E-06	3.33E-01	no
Napthalene	6.10E-04	tb/10 ⁶ scf	6.37E-06	2.29E-05	1.05E-06	3.33E+00	no
Nickel	2.10E-03	lb/10 ⁶ scf	2.88E-05	7.88E-05	3.63E-06	2,70E-05	yes
Pentane ·	2.60E+00	lb/10 ⁶ scf	3.57E-02	9.75E-02	4.50E-03	1.18E+02	no
Phenol	FNA	lb/10 ⁶ scf	FNA	FNA	FNA	1.27E+00	no
Selenium .	<2.4E-5	lb/10 ⁶ scf	3,29E-07	9.00E-07	4.15E-08	1,30E-02	no
Toluene	3.40E-03	lb/10 ⁸ scf	4.67E-05	1.28E-04	5.88E-06	2.50E+01	no
Vanadium	2.30E-03	lb/10 ⁶ scf	3.16E-05	8.63E-05	3.98E-06	3.00E-03	no
o-Xylene	FNA .	lb/10 ⁶ scf	FNA	FNA	FNA	2.90E+01	no
Zinc	2.90E-02	lb/10 ⁶ scf	3.98E-04	1.09E-03	5.02E-05	6,67E-01	no

98:

The annual natural gas consumption for this emission unit will be limited.

The annual production rate associated with this emission unit will be limited. Estimate

This emission unit vents to the atmosphere via two stacks. Stack gas flow data obtained from testing conducted in November 2001.

Emission Factors from AP-42 Chapter 1.4, "Natural Gas Combustion".

DAPA 58.01.01.585 and 586

DAPA 58.01.01.210.05(b)

"NA - Factor Not Available

s equivalent to operating 300 days per year at 90% of maximum hourly production rate.

Air Pollutant Emissions Burley Plant 2 - Prime 2 Dryer (D205 - D208)

Combustion Source Charac	teristics		Stack Da	ta ^c		
Burner Manufacturer	National	Proposed Stack Height (ft)	39.4	39.4	39.4	39.4
Model	None	Stack Diameter (ft)	4.78	4.78	4.78	4.78
Input Heat Capacity (BTU/hr)	48,000,000	Exit Gas Temperature (°F)	112.0	106.0	114.6	96.8
Fuel	Natural Gas	Exit Gas Moisture Content	5.51%	6,69%	6.39%	6.78%
Heating Value (BTU/scf)	1,020	Wet Actual Flow Rate (acfm)	40,152	42,877	35,678	40,006
Max Hourly Fuel Consumption (scf/hr)	47,059	Wet Standard Flow Rate (wscfm)	32,231	34,794	28,511	33,006
Annual Fuel Consumption (scf/yr)*	120,000,000	Dry Standard Flow Rate (dscfm)	30,455	32,466	26,689	30,768
		Stack Velocity (m/s)	11.38	12.16	10.12	11,34
Process Characteristi	CS	Stack Gas Pressure (mm Hg)	660.91	661.16	660.91	661.16
Max Hourly Production Rate (lb/hr)	45,000		Stack #1	Stack #2	Stack #3	Stack #4
Annual Production Rate (TPY) ^b	145,800				1	

Pollutant	Pollutant Source	Emission Factor [¢]	Emission Factor Unit	Potential Emissions (lb/hr)	Potentiai Emissions (TPY)	Potential Emissions (g/s)	Significant Level* (TPY)	Regulatory	Significant Contribution?
PM ₁₆	NG Combustion & Process	See PM	See PM	5.625	18.225	0.709	15	no	yes
SO ₂	NG Combustion	0.6	lb/10 ⁸ scf	0.028	0.036	0.004	40	yes	no
NO.	NG Combustion & Process	153	lb/10 ⁶ scf	7.200	9.180	0.907	40	no	no
CO	NG Combustion & Process	373	lb/10 ⁶ scf	17,553	22.380	2.212	100	no	no
voc	. NG Combustion	5.5	lb/10° scf	0.259	0.330	0.033	40	yes	no
Lead	NG Combustion	0.0005	lb/10° scf	2.35E-05	3.00E-05	2.96E-06	0,6	yes	no

Non-Criteria Po	ion-Criteria Pollutants with Significant Threshold												
		Emission	Emission	Polential	Potential Emissions	Potential Emissions		Regulatory					
Pollutant	Pollutant Source	Factor *	Factor Unit	Emissions (lb/hr)	(TPY)	(g/s)	(TPY)	Concern?'	Contribution?				
PM	NG Combustion & Process	0.25	lb/finished ton	5.625	18.225	0.709	25	no ·	no				
Beryllium	NG Combustion	<1.2E-5	lb/10 ⁶ scf	5.65E-07	7.20E-07	7.12E-08	0.0004	yes	no				
Mercury	NG Combustion	2.60E-04	ib/10 ⁶ scf	1.22E-05	1.56E-05	1.54E-06	0.1	yes	ne				

Other Poliutani	18			•		
Pollutant	Pollutant Source	Emission Factor ^d	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
тос	NG Combustion	11	lb/10 ⁸ scl	0.518	0.660	0.065
Methane	NG Combustion	2.3	lb/10 ⁶ scf	0.108	0.138	0.014
CO ₂	NG Combustion	120,000	lb/10 ⁶ scf	5647	7200	711.5
N₅O	NG Combustion	2.2	1b/10 ⁶ scl	0.104	0.132	0.013

Process Weight Rule										
		Potential	Stack#1	Stack #2	Stack #3			All Stacks		
Pollutant	Pollutant Source	Emissions (lb/hr)	Emissions (gr/dscf)	Emissions (gr/dscf)	Emissions (or/dscf)	Emissions (or/dscf)	(gr/dscf)	Meet Standard?		
PM	Process	5,625	0.022	0.020	0.025	0.021	0.2	Y 6 8		

PM Grain Loading Standard - Not Applicable

- (a) The annual natural gas consumption for this emission unit will be limited.
- (b) The annual production rate associated with this emission unit will be limited. Estimate is equivalent to operating 300 days per year at 90% of maximum hourly production rate.
- (c) This emission unit vents to the atmosphere via four stacks. Stack gas flow data obtained from testing conducted in November 2001.
- (d) Emission factors for NO_x and CO generated by the process and natural gas combustion based on April 1994 Ore-Ida Source Test
 (Ontario, OR Prime 1 North Dryer). Emission factors for PM generated by the process and natural gas combustion based on
 October 1994 Ore-Ida Source Test (Burley, ID Prime 1 Dryer), April 1995 Ore-Ida Source Test (Ontario, OR P1 Dryer) and February 1997
 Ore-Ida Source test (Ontario, OR P2 & P3 Dryers). As a conservative approach, emissions that were measured as PM during the source tests
 were considered to equal PM₁₉. Emission factors for other pollutants from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (e) IDAPA 58.01.01.006.92
- (f) IDAPA 58.01.01.221.01
- (g) IDAPA 58.01.01.710.08. Process weight rule standard is 0.2 gr/dscf for units constructed or modified prior to July 1, 2000,
- (h) IDAPA 58.01.01.676 or 677 The Prime 2 Dryer is a direct heat transfer system. Therefore, it does not satisfy the definition of "fuel burning equipment" as presented in IDAPA 58.01.01.006,41.
- * NA Not Applicable

Toxic Air Pollutant Emissions Burley Plant 2 - Prime 2 Dryer (D205 - D208)

Combustion Source Charac	teristics	· · · · · · · · · · · · · · · · · · ·	Stack Date	a [¢]		
mer	National	Proposed Stack Height (ft)	39.4	39.4	39.4	39.4
del	None	Stack Diameter (ft)	4.78	4.78	4.78	4.78
ut Heat Capacity (BTU/hr)	48,000,000	Exit Gas Temperature (°F)	112.0	106.0	114.6	96.8
el	Natural Gas	Exit Gas Moisture Content	5.51%	6.69%	6.39%	6.78%
ating Value (BTU/scf)	1,020	Wet Actual Flow Rate (acfm)	40,152	42,877	35,678	40,006
ix Hourly Fuel Consumption (scl/hr)	47.059	Wet Standard Flow Rate (wscfm)	32,231	34,794	28,511	33,006
nual Fuel Consumption (scf/yr)	120,000,000	Dry Standard Flow Rate (dscfm)	30,455	32,466	26,689	30,768
Unat Life Coustilibrou (2003)		Stack Velocity (m/s)	11.38	12.16	10.12	11.34
Process Characteristic	s	Stack Gas Pressure (mm Hg)	660.91	661.16	660.91	661.16
x Hourly Production Rate (lb/hr)	45,000		Stack #1	Stack #2	Stack #3	Stack #4
nual Production Rate (TPY) ^b	145,800	:				

Air Pollutants	Emission Factor	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)	Emission Limit ^s (lb/hr)	Modeling Required?
Pollutant Arsenic	2.00E-04	lb/10 ⁶ scf	9.41E-06	1,20E-05	1.19E-06	1.50E-06	ye*
	4.40E-03	lb/10 ⁶ scf	2.07E-04	2.64E-04	2.61E-05	3.30E-02	no
Barium	2.10E-03	lb/10 ⁶ scf	9.88E-05	1.26E-04	1.25E-05	8.00E-04	no
Benzene	<1.2E-5	1b/10 ⁶ scf	5.65E-07	7.20E-07	7.12E-08	2.80E-05	no
Beryllium	<1.2E-6	lb/10 ⁶ scf	5.65E-08	7.20E-08	7.12E-09	2.00E-06	no
Benzo(a)pyrene	FNA	lb/10 ⁶ scf	FNA	FNA	FNA	2.80E-02	no
Bis (2-ethylhexyl)phthalate Cadmium	1.10E-03	lb/10 ⁶ scf	5.18E-05	6.60E-05	6.52E-06	3.70E-06	Y * \$
Chromium	1.40E-03	lb/10 ⁶ scf	6.59E-05	8.40E-05	8.30E-06	3.30E-02	no
Cobalt	8.40E-05	Ib/10 ⁶ scf	3.95E-06	5.04E-06	4.98E-07	3.30E-03	no
Copper	8.50E-04	lb/10 ⁶ scf	4.00E-05	5.10E-05	5.04E-06	3.33E-01	no
Dibutylphthalate	FNA	1b/10 ⁶ scf	FNA	FNA	FNA .	6.70E-02	ne
Dichlorobenzene	1,20E-03	lb/10 ⁶ scf	5.65E-05	7,20E-05	7.12E-06	2.00E+01	no
Ethylbenzene	FNA	lb/10 ⁸ scf	FNA .	FNA	FNA	2.90E+01	no
Fluorene	2.80E-06	lb/10 ⁶ scf	1.32E-07	1.68E-07	1.66E-08	1.33E-01	no
Formaldehyde	7.50E-02	lb/10 ⁶ scf	3.53E-03	4.50E-03	4.45E-04	5.10E-04	yes
) exane	1.80E+00	lb/10 ⁶ scf	8.47E-02	1.08E-01	1.07E-02	1.20E+01	no
Manganese	3.80E-04	lb/10 ⁶ scf	1.79E-05	2.28E-05	2.25E-06	3.33E-01	no
Mercury	2.60E-04	lb/10 ⁶ scf	1.22E-05	1.56E-05	1.54E-06	3,00E-03	no
Molvhdenum	1.10E-03	lb/10 ⁶ scf	5.18E-05	6.60E-05	6.52E-06	3.33E-01	no
Napthalene	6.10E-04	lb/10 ⁸ scf	2.87E-05	3.66E-05	3.62E-06	3.33E+00	no
Nickel	2.10E-03	lb/10 ⁶ scf	9.88E-05	1,26E-04	1.25E-05	2.70E-05	yes
Pentane	2.60E+00	lb/10 ⁸ scf	1.22E-01	1.56E-01	1.54E-02	1.18E+02	no
Phenol	FNA	lb/10 ⁶ scf	FNA	FNA	FNA	1.27E+00	no
Selenium	<2.4E-5	lb/10 ⁶ scf	1.13E-06	1.44E-06	1.42E-07	1.30E-02	no
Toluene	3.40E-03	lb/10 ⁶ scf	1.60 E-04	2.04E-04	2.02E-05	2.50E+01	no
Vanadium	2.30E-03	lb/10 ⁶ scf	1.08E-04	1.38E-04	1.36E-05	3.00E-03	no
o-Xylene	FNA	lb/10 ⁶ scf	FNA	FNA	FNA	2.90E+01	
Zinc	2.90E-02	lb/10 ⁶ scf	1.36E-03	1.74E-03	1.72E-04	6.67E-01	no

es:

The annual natural gas consumption for this emission unit will be limited.

The annual production rate associated with this emission unit will be limited. Estimate

s equivalent to operating 300 days per year at 90% of maximum hourly production rate.

This emission unit vents to the atmosphere via four stacks. Stack gas flow data obtained from testing conducted in November 2001.

Emission Factors from AP-42 Chapter 1.4, "Natural Gas Combustion".

IDAPA 58.01.01.585 and 586

DAPA 58.01.01.210.05(b)

FNA - Factor Not Available

Air Pollutant Emissions **Fryers**

Emission Source	Pollutant	Emission Factor ^a (lb/finished ton)	Maximum Production Rate (finished lb/hr)		Emission Rate ^b (TPY)	Significant Level ^e (TPY)	Below Regulatory Concern?d	Significant?°	Allowable PM Emissions (gr/dscf)	Meets Standard?* (gr/dscf)
Parfry Fryer Alr Washer (F108) PM ₁₀ VOC	0.51	5,100	1.301	4.214	15	no	no	0.026	yes	
	0.15	5,100	0.383	1.239	40	yes	. uo	NA	NA	
Tot Fryer Air Washer (F103) PM ₁₀ VOC	0.51	16,000	4,080	13.219	15	no	no	0.043	· yes	
	voc	0.15	16,000	1.200	3.888	· 40	yes	no	NA	NA
Prime 1 Fryer	PM ₁₀	0.10	53,500	2.675	8.667	15	no	no	0.053	yes
Air Washer (F104)	voc	0.10	53,500	2.675	8.667	40	no	no	NA NA	NA
Air Wacher (F20A)	PM ₁₀ .	0.10	45,000	2.250	7.290	15	no	по	0.023	yes
	voc	0.10	45,000	2.250	7.290	40	no	no	NA	NA

Emission Source	Stack Height (ft)	Stack Diameter (ft)	Exit Gas Temperature (°F)	Exit Gas Moisture	Wet Flow Rate (acfm)	Dry Flow Rate (dscfm)	Stack Gas Velocity (m/s)	Stack Gas Pressure (mm Hg)
Parfry Fryer Air Washer (F108)	52.5	2.61	101.0	5.58%	7,587	5,886	7.20	663.45
Tot Fryer Air Washer (F103)	53.6	3.71	131.0	17.89%	17,268	11,059	8.13	663.45
Prime 1 Fryer Air Washer (F104)	59.0	3.12	175.1	39.40%	13,390	5,887	8.91	663.19 658.11
Prime 2 Fryer Air Washer (F204)	44.6	3.17	156.4	28,75%	20,729	11,262	13.38	636.11

- (a) Emission factors for Parfry Fryer and Tot Fryer based on October 1994 Ore-ida Source Test (Plover, WI P2 Specialty 3 Fryer with Air Washer) Emission factors for Prime 1 Fryer and Prime 2 Fryer based on October 1994 Ore-Ida Source Test (Burley, ID - Prime 1 Fryer with Air Washer) and April 1994 Ore-Ida Source Test (Ontario, OR - Prime 1 French Fryer with Air Washer). As a conservative approach, emissions that were measured as PM during the source tests were considered to equal $\ensuremath{\text{PM}_{\text{10}}}$
- (b) Annual emissions based on limited annual production rate that is equivalent to operating 300 days per year at 90% of maximum hourly production rate.
- (c) IDAPA 58.01.01.006.92
- (e) IDAPA 58.01.01.710.08. Process weight rule standard is 0.2 gr/dscf for units constructed or modified prior to July 1, 2000.
- (f) Stack gas flow data obtained from testing conducted in November 2001. Grain Loading Standard - IDAPA 58.01.01.676 is not applicable because these emission sources are not "fuel burning equipment".

Air Pollutant Emissions Burley Plant 1 - Murray 1 Boiler (B101)

Combustion Source Charac	terist ics	Stack Data	
Boiler Manufacturer	Murray Boiler	Stack Height (ft)	40.7
Burner Model	Coen DAZ	Stack Diameter (ft)	5.00
Input Heat Capacity (BTU/hr)	100,000,000	Exit Gas Temperature (°F)	308
Fuel	Natural Gas	Wet Actual Flow Rate (acfm)	29,882
Heating Value (BTU/scf)	1,020	Wet Standard Flow Rate (wscfm)	17,683
Max Hourly Fuel Consumption (scf/hr)	98,039	Dry Standard Flow Rate (dscfm)	14,517
Annual Fuel Consumption (scf/yr)*	"Bubbled"	Grain Loading Flow Rate (dscfm)	19,691
Puniosi i do la companya de la compa		Stack Velocity (m/s)	7.73
Site information		Fd (dscf stack gas/BTU)	0.00871
Burley Barometric Pressure (mm Hg)	654.18	Fw (wscf stack gas/BTU)	0.01061

Pollutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Poten tial Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
PM ₁₀	NG Combustion	7.6	lb/10 ⁶ scf	0.745		0.094
SO₂	NG Combustion	0,6	lb/10 ⁸ scf	0.059	*	0.007
NO.	NG Combustion	100	lb/10 ⁶ scf	9,804		1.235
СО	NG Combustion	84	lb/10 ⁶ scf	8.235	*	1.038
VOC	NG Combustion	5.5	lb/10 ⁶ scf	0.539	*	0.068
Lead	NG Combustion	0.0005	lb/10° scf	4.90E-05		6.18E-06

on-Criteria Po	liutants with Signifi	cant Thresho	old			
Poliutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Poten tial Emissions (lb/hr)	Potential Emissiona (TPY)	Potential Emissions (g/s)
PM	NG Combustion	See PM ₁₀	See PM ₁₀	0.745	•	9.39E-02
Bervilium	NG Combustion	<1.2E-5	lb/10 ⁶ scf	1.18E-06	. *	1.48E-07
Mercury	NG Combustion	2.60E-04	lb/10 ⁸ scf	2.55E-05	•	3.21E-06

iher Pollutani Poliutani	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
TOC	NG Combustion	11	lb/10° scf	1.08	•	0.136
Methane	NG Combustion	2.3	lb/10 ⁶ scf	0.225		0.028
CO ₂	NG Combustion	120,000	lb/10 ⁶ scf	11,765	*	1,482
N ₂ O	NG Combustion	2.2	lb/10 ⁶ scf	0.216		0.027

PM Grain Loadi	ng Stand ard^e				
		Potential Emissions	Grein Load @ 3% Oxygen	PM Grain Standard ^e	Meets
Pollutant	Pollutant Source	(lb/hr)	(gr/dscf)	(gr/dscf)	Standard?
PM	NG Combustion	0.745	0.004	0.015	· yes

Process Weight Rule - Not Applicable

- (a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be limited, rather than the fuel consumption of the individual boilers. Detailed annual emission estimates for the "Boiler Bubble" are presented in a separate spreadsheet.
- (b) Emission factors from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (c) IDAPA 58.01.01.677
- (d) IDAPA 58.01.01.710.03 The Murray 1 Boller (B101) is subject to IDAPA 58.01.01.677; therefore, Subsection 710.08 is not applicable.

Toxic Air Pollutant Emissions Burley Plant 1 - Murray 1 Boiler (B101)

acteristics	Stack Data	
Murray Boiler	Stack Height (ft)	40.7
Coen DAZ	Stack Diameter (ft)	5.00
100,000,000	Exit Cas Temperature (°F)	308
Natural Gas	Wet Actual Flow Rate (acfm)	29,882
1,020	Wet Standard Flow Rate (wscfm)	17,683
98,039	Dry Standard Flow Rate (dscfm)	14,517
"Bubbled"	Grain Loading Flow Rate (dscfm)	19,691
	Stack Velocity (m/s)	7.73
1	Fd (dscf stack gas/BTU)	0.00871
654.18	Fw (wscf stack gas/BTU)	0.01061
	Murray Boiler Coen DAZ 100,000,000 Natural Gas 1,020 98,039 "Bubbled"	Murray Boiler Coen DAZ 100,000,000 Exit Gas Temperature (°F) Natural Gas 1,020 98,039 "Bubbled" Grain Loading Flow Rate (dscfm) Stack Velocity (m/s) Fd (dscf stack gas/BTU)

c Air Pollutants	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (g/s)	Emission Limit ^e (lb/hr)	Modeling Required?
Arsenic	2.00E-04	lb/10 ⁶ scf	1.96E-05	2.47E-06	1.50E-06	yes
Berium	4.40E-03	lb/10 ⁶ scf	4.31E-04	5.44E-05	3.30E-02	no
Benzene	2,10E-03	lb/10 ⁶ scf	2.06E-04	2.59E-05	8.00E-04	no
Beryllium	<1,2E-5	lb/10 ⁶ scf	1.18E-06	1.48E-07	2.80E-05	no
Benzo(a)pyrene	<1.2E-6	ib/10 ⁶ scf	1.18E-07	1.48E-08	2.00E-06	no
Bis (2-ethylhexyl)phthalate	FNA	lb/10 ⁶ scf	FNA	FNA	2.80E-02	no
Cadmium	1.10E-03	lb/10 ⁶ scf	1.08E-04	1.36E-05	3.70E-06	yes
Chromium	1,40E-03	lb/10 ⁶ scf	1.37E-04	1.73E-05	3.30E-02	no
Coball	8.40E-05	lb/10 ⁶ scf	8.24E-06	1.04E-06	3.30E-03	no
Copper	8.50E-04	ib/10 ⁶ scf	8.33E-05	1.05E-05	3.33E-01	no
Dibutylphthalate	FNA	lb/10 ⁶ scf	FNA	FNA	6.70E-02	no
Dichlorobenzene	1,20E-03	lb/10 ⁶ scf	1,18E-04	1.48E-05	2.00E+01	no
Ethylbenzene	FNA	lb/10 ⁵ scf	FNA	FNA	2.90E+01	no
Fluorene	2.80€-06	lb/10 ⁶ scf	2.75E-07	3.46E-08	1,33E-01	no
Formaldehyde	7.50E-02	lb/10 ⁶ scf	7.35E-03	9.26E-04	5.10E-04	yes
Hexane	1.80E+00	lb/10 ⁶ scf	1.76E-01	2,22E-02	1.20E+01	no
Manganese	3.80E-04	lb/10 ⁸ scf	3.73E-05	4.69E-06	3.33E-01	no
Mercury	2.60E-04	1b/10 ⁵ scf	2.55E-05	3.21E-06	3.00E-03	no
Molybdenum	1.10E-03	lb/10 ⁶ scf.	1.08E-04	1.36E-05	3.33E-01	no
Napthalene	6.10E-04	lb/10 ⁶ scf	5.98E-05	7.54E-06	3.33E+00	no
Nickel	2.10E-03	lb/10 ⁶ scf	2.06E-04	2.59E-05	2.70E-05	yes
Pentane	2.60E+00	lb/10 ⁸ scf	2.55E-01	3.21E-02	1.18E+02	no
Phenol	FNA	lb/10 ⁶ scf	FNA	FNA	1.27E+00	no
Selenium	<2.4E-5	Ib/10 ⁶ scf	2.35 E-06	2.96E-07	1.30E-02	no
Toluene	3,40E-03	lb/10 ⁶ scf	3.33E-04	4.20E-05	2.50E+01	no
Venadium	2.30E-03	Ib/10 ⁶ scf	2.25E-04	2.84E-05	3.00E-03	no
o-Xylene	FNA	lb/10 ⁶ scf	FNA	FNA	2.90E+01	no
Zinc	2.90E-02	lb/10 ⁶ scf	2.84E-03	3.58E-04	6.67E-01	no

- (a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be limited, rather than the fuel consumption of the individual boilers. Detailed annual emission estimates for the "Boiler Bubble" are presented in a separate spreadsheet.
- (b) Emission Factors from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (c) IDAPA 58.01.01.585 and 586
- (d) IDAPA 58.01.01.210.05(b)
- * FNA Factor Not Available

Air Pollutant Emissions Burley Plant 1 - Nebraska 1 Boiler (B102)

Combustion Source Charac	teristi cs	Stack Data	
Boiler Manufacturer	Nebraska Boiler	Stack Height (ft)	64.9
Burner Model	Coen DAZ	Stack Diameter (ft)	4.00
Input Heat Capacity (BTU/hr)	95,580,000	Exit Gas Temperature (°F)	308
Fuel	Natural Gas	Wet Actual Flow Rate (acfm)	28,561
Heating Value (BTU/scf)	1,020	Wet Standard Flow Rate (wscfm)	16,902
Max Hourly Fuel Consumption (scf/hr)	93,706	Dry Standard Flow Rate (dscim)	13,875
Annual Fuel Consumption (sc/yr)*	"Bubbled"	Grain Loading Flow Rate (dscfm)	18,821
Literanges a water and a service and a servi		Stack Velocity (m/s)	11.54
Site Information		Fd (dscf stack gas/BTU)	0.00871
Burley Barometric Pressure (mm Hg)	654.18	Fw (wscf stack gas/BTU)	0.01061

Pollutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
PM ₁₀	NG Combustion	7.6	lb/10 ⁶ scf	0.712	•	0.090
SO ₂	NG Combustion	0.6	lb/10 ⁶ scf	0.056		0.007
NO,	NG Combustion	100	lb/10 ⁶ scf	9.371		1.181
co	NG Combustion	84	lb/10 ⁶ scf	7.871		0.992
voc	NG Combustion	5.5	lb/10 ⁶ scf	0.515	•	0.965
Lead	NG Combustion	0.0005	lb/10 ⁶ scf	4.69E-05	•	5.90E-06

Non-Criteria Po	llutants with Signifi	cant Thresho	ild	· · · · · · · · · · · · · · · · · · ·		-
Pollutant	Poliutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (ib/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
PM	NG Combustion	See PM ₁₀	See PM ₁₀	0.712	•	8.97E-02
Bervlium	NG Combustion	<1.2E-5	lb/10 ⁶ scf	1.12E-06		1.42E-07
Mercury	NG Combustion	2.60E-04	lb/10 ⁶ scf	2.44E-05	*	3.07E-06

Pollutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
TOC	NG Combustion	11	lb/10 ⁶ scf	1.03	•	0.130
Methane	NG Combustion	2,3	lb/10 ⁶ scf	0.216		0.027
CO ₂	NG Combustion	120,000	lb/10 ⁶ scf	11,245	•	1,417
N₂O	NG Combustion	2.2	lb/10 ⁶ scf	0.206	Ð	0.026

PM Grain Loadi	PM Grain Loading Standard ^e									
		Potential Emissions	Grain Load @ 3% Oxygen	PM Grain Standard ^e	Meets					
Pollutant	Pollutant Source	(lb/hr)	(gr/dscf)	(gr/dscf)	Standard?					
PM	NG Combustion	0,712	0.004	0.015	yes					

Process Weight Rule - Not Applicable

- (a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be limited, rather than the fuel consumption of the individual boilers. Detailed annual emission estimates for the "Boiler Bubble" are presented in a separate spreadsheet.
- (b) Emission factors from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (c) IDAPA 58.01.01.676
- (d) IDAPA 58.01.01.710.03 The Nebraska 1 Boiler (B102) is subject to IDAPA 58.01.01.676; therefore, Subsection 710.08 is not applicable.

Toxic Air Pollutant Emissions Burley Plant 1 - Nebraska 1 Boiler (B102)

Combustion Source Char	acteristics	Stack Date	
Boller Manufacturer	Nebraska Boiler	Stack Height (ft)	64.9
Burner Model	Coen DAZ	Stack Diameter (ft)	4,00
Input Heat Capacity (BTU/htr)	25,580,000	Exit Gas Temperature (°F)	308
Fuel	Natural Gas	Wet Actual Flow Rate (acfm)	28,561
Heating Value (BTU/scf)	1,020	Wet Standard Flow Rate (wscfm)	16,902
Max Hourly Fuel Consumption (scf/hr)	93,706	Dry Standard Flow Rate (dscfm)	13,875
Annual Fuel Consumption (scf/yr)*	"Bubbled"	Grain Loading Flow Rate (dscfm)	18,821
Little Land Control Land		Stack Velocity (m/s)	11,54
Site Information		Fd (dscf stack gas/BTU)	0.00871
Burley Barometric Pressure (mm Hg)	654.18	Fw (wscl stack gas/BTU)	0.01061

	1	Emission	Potential	Potential	1 1	
	Emission	Factor	Emissions	Emissions	Emission Limit	Modeling
Poliutant	Factor*	Unit	(ID/hr)	(g/s)	(lb/hr)	Required?
Arsenic	2.00E-04	ib/10 ⁶ scf	1.87E-05	2.36E-06	1.50E-06	yes
Barium	4.40E-03	lb/10 ⁶ scf	4.12E-04	5.20E-05	3.30E-02	no
Benzene	2.10E-03	lb/10 ⁸ scf	1.97E-04	2.48E-05	8.00E-04	no
. Beryllium	<1.2E-5	lb/10 ⁶ scf.	1.12E-06	1.42E-07	2.80E-05	no
Benzo(e)pyrene	<1.2E-6	lb/10 ⁶ scf	1.12E-07	1.42E-08	2.00E-06	no
Bis (2-ethylhexyl)phthalate	FNA	lb/10 ⁶ scf	FNA	FNA	2.80E-02	no
Cadmium	1.10E-03	lb/10 ⁶ scf	1.03E-04	1.30E-05	3.70E-06	yes
Chromium	1,40E-03	lb/10 ⁶ scf	1.31E-04	1.65E-05	3.30E-02	no
Cobalt	8.40E-05	lb/10 ⁶ scf	7.87E-06	9.92E-07	3.30E-03	no
Copper	8.50E-04	1b/10 ⁶ scf	7.97E-05	1.00E-05	3.33E-01	no
Dibutylphthelate	FNA	lb/10 ⁸ scf	FNA	FNA	6.70E-02	no
Dichlorobenzene	1.20E-03	lb/10 ⁸ scf	1,12E-04	1.42E-05	2.00E+01	no
Ethylbenzene	FNA	lb/10 ⁶ scf	FNA	FNA	2.90E+01	no
Fluorene	2.80E-06	lb/10 ⁶ scf	2.62E-07	3.31E-08	1.33E-01	no
Formaldehyde	7.50E-02	lb/10 ⁶ scf	7.03E-03	8.86E-04	5.10E-04	yes
Hexane	1.80E+00	lb/10 ⁶ scf	1.69E-01	2.13E-02	1.20E+01	no
Manganese	3.80E-04	lb/10 ⁶ scf	3.56E-05	4.49E-06	3.33E-01	no
Mercury	2.60E-04	lb/10° scf	2.44E-05	3.07E-06	3.00E-03	no
Molybdenum	1,10E-03	ib/10 ⁶ scf	1.03E-04	1,30E-05	3.33E-01	no
Napthalene	6.10E-04	lb/10 ⁶ scf	5.72E-05	7.20E-06	3.33E+00	no
Nickel	2.10E-03	lb/10 ⁶ scf	1.97E-04	2.48E-05	2.70E-05	yes
Pentane .	2.60E+00	lb/10 ⁶ scf	2.44E-01	3.07E-02	1.18E+02	no
Phenol	FNA	lb/10 ⁶ scf	FNA	FNA	1.27E+00	no
Selenium	<2.4E-5	lb/10 ⁶ scf	2.25E-06	2.83E-07	1.30E-02	no
Toluene	. 3.40E-03	lb/10 ⁶ scf	3.19E-04	4.01E-05	2.50E+01	no
Vanadium	2.30E-03	lb/10 ⁵ scf	2.16E-04	2.72E-05	3.00E-03	no
o-Xylene	FNA	lb/10 ⁸ scf	FNA	FNA	2.90E+01	no
Zinc	2.90E-02	lb/10 ⁶ scf	2.72E-03	3.42E-04	6.67E-01	no

⁽a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be limited, rather than the fuel consumption of the individual boilers. Detailed annual emission estimates for the "Boiler Bubble" are presented in a separate spreadsheet.

⁽b) Emission Factors from AP-42 Chapter 1.4, "Natural Gas Combustion".

⁽c) IDAPA 58,01.01.585 and 586

⁽d) IDAPA 58.01.01.210.05(b)

FNA - Factor Not Available

Air Pollutant Emissions Burley Plant 2 - Nebraska 2 Boiler (B202)

teristic s	Stack Data	
Nebraska Boiler	Stack Height (ft)	66.8
Coen DAZ	Stack Diameter (ft)	3.00
78,050,000	Exit Gas Temperature (°F)	308
Natural Gas	Wet Actual Flow Rate (acfm)	23,323
1,020	Wet Standard Flow Rate (wscfm)	13,802
76,520	 Dry Standard Flow Rate (dscfm) 	11,330
"Bubbled"	Grain Loading Flow Rate (dscfm)	15,369
	Stack Velocity (m/s)	16.76
	Fd (dscf stack gas/BTU)	0.00871
654.18	Fw (wscf stack gas/BTU)	0.01061
	Coen DAZ 78,050,000 Natural Gas 1,020 76,520 "Bubbled"	Nebraska Boiler Stack Height (ft) Coen DAZ Stack Diameter (ft) 78,050,000 Exit Gas Temperature (°F) Natural Gas Wet Actual Flow Rate (acfm) 1,020 Wet Standard Flow Rate (wscfm) 76,520 Dry Standard Flow Rate (dscfm) "Bubbled" Grain Loading Flow Rate (dscfm) Stack Velocity (m/s) Fd (dscf stack gas/BTU)

Pollutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
PM ₁₀	NG Combustion	7.6	lb/10 ⁸ scf	0.582	#	0.073
SO ₂	NG Combustion	0.6	lb/10 ⁸ scf	0.046	. •	0.006
NO,	NG Combustion	100	lb/10 ⁶ scf	7.652	*	0.964
CO	NG Combustion	84	lb/10 ⁶ scf	6.428		0.810
voc	NG Combustion	- 5.5	lb/10 ⁶ scf	0.421	*	0.053
Lead	NG Combustion	0.0005	lb/10 ⁶ scf	3.83E-05		4.82E-06

ion-Criteria Po	llutents with Signifi	cant Thresho	ld			
Pollutani	Pollutant Source	Emission Factor	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential . Emissions (g/s)
PM	NG Combustion	See PM ₁₀	See PM ₁₀	0.582	. *	7.33E-02
Beryllium	NG Combustion	<1.2E-5	lb/10 ⁶ scf	9.18E-07	•	1.16E-07
Mercury	NG Combustion	2.60E-04	lb/10 ⁸ scf	1.99E-05	. *	2.51E-06

Pollutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
TOC	NG Combustion	11	lb/10 ⁸ scf	0.84	•	0.106
Methane	NG Combustion	2.3	Ib/10° scf	0.176	*	0.022
CO ₂	NG Combustion	120,000 -	lb/10° scf	9,182	*	1,157
· N _z O	NG Combustion	2.2	lb/10° scf	· 0,168	*	0.021

PM Grain Loadi	PM Grain Loading Standard ^e									
		Potential Emissions	Grain Load @ 3% Oxygen	PM Grein Stendard ^c	Meets					
Pollutant	Pollutant Source	(lb/hr)	(gr/dscf)	(gr/dscf)	Standard?					
PM	NG Combustion	0.582	0.004	0.015	yes_					

Process Weight Rule - Not Applicable

- (a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be limited, rather than the fuel consumption of the individual boilers. Detailed annual emission estimates for the "Boiler Bubble" are presented in a separate spreadsheet.
- (b) Emission factors from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (c) IDAPA 58.01.01.676
- (d) IDAPA 58.01.01.710.03 The Nebraska 2 Boiler (B202) is subject to IDAPA 58.01.01.676; therefore, Subsection 710.08 is not applicable.

APPENDIX B Modeling Memo

Toxic Air Pollutant Emissions Burley Plant 2 - Nebraska 2 Boiler (B202)

Combustion Source Char	acteristi cs	Stack Data	
Boiler Manufacturer	Nebraska Boiler	Stack Height (ft)	66.8
Burner Model	Coen DAZ	Stack Diameter (ft)	3
Input Heat Cepacity (BTU/hr)	78,050,000	Exit Gas Temperature (°F)	308
Fuel	Natural Gas	Wet Actual Flow Rate (acfm)	23,323
Heating Value (BTU/scf)	1.020	Wet Standard Flow Rate (wscfm)	13,802
Max Hourly Fuel Consumption (scf/fir)	76.520	Dry Standard Flow Rate (dscfm)	11,330
Annual Fuel Consumption (sc//yr)*	"Bubbled"	Grain Loading Flow Rate (dscfm)	15,369
Allina roe Consumptor (const.)		Stack Velocity (m/s)	16.76
Site information		Fd (dscf stack gas/BTU)	0.00871
Burley Barometric Pressure (mm Hg)		Fw (wscf stack gas/BTU)	0.01061

c Air Pollutants		Emission	Potential	Potential	Emission	
•	Emission	Factor	Emissions	Emissions	i_irrif ^e	Modeling
Poliutent	Factor ^b	Unit	(lb/hr)	(g/s)	(lb/hr)	Required?
Arsenic	2.00E-04	ib/10 ⁶ scf	1.53E-05	1.93E-06	1.50E-06	yes
Barlum	4.40E-03	Ib/10 ⁶ scf	3.37E-04	4.24E-05	3.30E-02	no
Benzene	2.10E-03	lb/10 ⁶ scf	1.61E-04	2.02E-05	8,00 E-04	no
Beryfflum	<1.2E-5	lb/10 ⁶ scf	9.18E-07	1.16E-07 .	2.80E-05	no
Benzo(a)pyrene	<1.2E-6	lb/10 ⁶ scf	9.18E-08	1.16E-08	2.00E-06	no_
Bis (2-ethylhexyl)phthalate	FNA	lb/10 ⁶ scf	FNA	FNA	2.80E-02	no
Cadmium	1.10E-03	lb/10 ⁶ scf	8.42E-05	1.06E-05	3.70E-06	yes_
Chromlum	1.40E-03	1b/10 ⁶ scf	1.07E-04	1.35E-05	3.30E-02	no
Cobalt	8.40E-05	Ib/10 ⁶ scf	6.43E-06	8.10E-07	3.30E-03	no
Copper	8.50E-04	lb/10 ⁸ scf	6.50E-05	8.20E-06	3.33E-01	no
Dibutylphthelete	FNA	lb/10 ⁶ scf	FNA	FNA	6.70E-02	no.
Dichlorobenzene	1,20E-03	lb/10 ⁸ scf	9.18E-05	1.16E-05	2.00E+01	. no
Ethylbenzene	FNA	lb/10 ⁶ scf	FNA	FNA	2.90E+01	-no
Fluorene	2.80E-06	lb/10 ⁶ scf	2.14E-07	· 2.70E-08	1.33E-01	no
Formaklehyde	7.50E-02	lb/10 ⁶ scf	5.74E-03	7.23E-04	5.10E-04	yes.
Hexane	1.80E+00	lb/10 ⁶ scf	1.38E-01	1.74E-02	1.20E+01	no
Manganese	3.80E-04	lb/10 ⁶ scf	2.91E-05	3.66E-06	3.33E-01	no
Mercury	2.60E-04	lb/10 ⁶ scf	1.99E-05	2.51E-06	3.00E-03	no
Molybdenum	1.10E-03	lb/10 ⁶ scf	8.42E-05	1.06E-05	3.33E-01	no
Napthalene	6.10E-04	lb/10 ⁶ scf	4.67E-05	5.88E-06	3.33E+00	no
Nickel	2.10E-03	lb/10 ⁶ scf	1.61E-04	2.02E-05	2.70E-05	yes
Pentane .	2.60E+00	lb/10 ⁶ scf	1.99E-01	2,51E-02	1.18E+02	no
Phenol	FNA	lb/10 ⁶ scf	FNA	FNA	1.27E+00	no
Selenium	<2.4E-5	lb/10 ⁶ scf	1.84E-06	2.31E-07	1.30E-02	no
Toluene	3.40E-03	lb/10 ⁶ scf	2.60E-04	3.28E-05	2.50E+01	no
Vanadium	2.30E-03	lb/10 ⁶ scf	1.76E-04	2.22E-05	3.00 E-03	no
o-Xylene	FNA	lb/10 ⁶ scf	FNA	FNA	2.90E+01	no
Zinc	2.90E-02	lb/10 ⁶ scf	2.22E-03	2.80E-04	6.67E-01	no

⁽a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be limited, rather than the fuel consumption of the individual boilers. Detailed annual emission estimates for the "Boiler Bubble" are presented in a separate spreadsheet.

⁽b) Emission Factors from AP-42 Chapter 1.4, "Natural Gas Combustion".

⁽c) IDAPA 58.01.01.585 and 586

⁽d) IDAPA 58.01.01.210.05(b)

FNA - Factor Not Available

Air Pollutant Emissions Burley Plant 2 - Murray 2 Boiler (B203)

Combustion Source Charac	teristics	Stack Data	
Boiler Manufacturer	Murray Boller	Stack Height (ft)	37.9
Burner Model	Coen DAZ	Stack Diameter (fl)	3.00
Input Heat Capacity (BTU/hr)	39,100,000	Exit Gas Temperature (*F)	308
Fuel	Natural Gas	Wet Actual Flow Rate (acfm)	11,684
Heating Value (BTU/scf)	1,020	Wet Standard Flow Rate (wscfm)	6,914
Max Hourly Fuel Consumption (scf/hr)	38,333	Dry Standard Flow Rate (dscfm)	5,676
Annual Fuel Consumption (scf/yr)*	"Bubbled"	Grain Loading Flow Rate (dscfm)	7,699
Partition 1 mar a series		Stack Velocity (m/s)	8.39
Site Information		Fd (dscf stack gas/BTU)	0.00871
Burley Barometric Pressure (mm Hg)	654.18	Fw (wscf stack gas/BTU)	0.01061

Pollutant	Poliutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
PM ₁₀	NG Combustion	7.6	lb/10 ⁶ scf	0.291		0.037
SO₂	NG Combustion	0,6	lb/10 ⁶ scf	0.023	*	0.003
NO.	NG Combustion	100	lb/10 ⁶ scf	3.833		0.483
CO	NG Combustion	84	lb/10 ^e scf	3.220	ė	0.406
VOC	NG Combustion	5.5	lb/10 ⁸ scf	0.211		0.027
Lead	NG Combustion	0.0005	lb/10 ⁶ scf	1.92E-05	*	2.42E-06

on-Criteria Po	llutants with Signifi	cant Thresho	old .			
Pollutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
PM	NG Combustion	See PM ₁₀	See PM ₁₀	0.291	* ·	3.67E-02
Beryllium	NG Combustion	<1.2E-5	lb/10 ⁶ scf	4.60E-07	. *	5.80E-08
Mercury	NG Combustion	2.60E-04	lb/10 ⁶ scf	9.97E-06		1,26E-06

Pollutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)
тос	NG Combustion	11	lb/10 ⁶ scf	0.42	•	0.053
Methane	NG Combustion	2.3	lb/10 ⁵ scf	0.088		0.011
CO ₂	NG Combustion	120,000	lb/10 ⁶ scf	4,600	•	580
N ₂ O	NG Combustion	2.2	lb/10 ⁶ scf	0.084		0.011

PM Grain Load	ng Stand ard^e				
	Pollutent Source	Potential Emissions (lb/hr)	Grain Load @ 3% Oxygen	PM Grain Standard ^c (cr/dscf)	Meets Standard?
Pollutant	FUNCION SOUICE	(8,311)	(gr/dscf)	(QI/OSCI)	OMINAINA
PM	NG Combustion	0.291	0.004	0.015	yes

Process Weight Rule - Not Applicable

- (a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be limited, rather than the fuel consumption of the individual boilers. Detailed annual emission estimates for the "Boiler Bubble" are presented in a separate spreadsheet.
- (b) Emission factors from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (c) IDAPA 58.01.01.677
- (d) IDAPA 58.01.01.710.03 The Murray 2 Boller (B202) is subject to IDAPA 58.01.01.677; therefore, Subsection 710.08 is not applicable.

Toxic Air Pollutant Emissions Burley Plant 2 - Murray 2 Boiler (B203)

Combustion Source Chara	ecteristi cs	Stack Data	
Boiler Manufacturer	Murray Boiler	Stack Height (ft)	37.9
Burner Model	Coen DAZ	Stack Diameter (ft)	3.00
Input Heat Capacity (BTU/hr)	39,100,000	Exit Gas Temperature (°F)	308
Fuel	Natural Gas	Wet Actual Flow Rate (acfm)	11,684
Heating Value (BTU/scf)	1,020	Wet Standard Flow Rate (wscfm)	6,914
Max Hourly Fuel Consumption (scf/hr)	38,333	Dry Standard Flow Rate (dscfm)	5,676
Annual Fuel Consumption (sc//yr)*	"Bubbled"	Grain Loading Flow Rate (dscfm)	7,699
William I par parent ham a frame.		Stack Velocity (m/s)	8.39
Site information		Fd (dscf stack gas/BTU)	0.00871
Burley Barometric Pressure (mm Hg)	654.18	Fw (wscf stack gas/BTU)	0.01061

	1	Emission	Potential	Potential	Emission	
· .	Emission	Factor	Emissions	Potential Emissions	Limit	Modeling
Poliutani	Factor ^b .	Unit	(lb/hr)	(g/s)	(lb/br)	Required?
Arsenic	2,00E-04	lb/10 ⁶ scf	7.67E-06	9.66E-07	1.50E-06	yes
Barium	4.40E-03	lb/10 ⁶ scf	1.69E-04	2,13E-05	3.30E-02	no
Benzene	2,10E-03	lb/10 ⁸ scf	8.05 E-0 5	1.01E-05	8.00E-04	no
Beryllum	<1.2E-5	lb/10 ⁶ scf	4.60E-07	5.80 E-08	2.80E-05	no
Benzo(a)pyrene	<1.2E-6	lb/10 ^e scf	4.60E-08	5.80 E-09	2.00E-06	no
Bis (2-ethylhexyl)phthalate	FNA	lb/10 ⁶ scf	FNA	FNA	2.80E-02	no
Cadmium	1,10E-03	lb/10 ⁸ scf	4.22E-05	5.31E-06	3.70E-06	yes
Chromium	1.40E-03	lb/10 ⁸ scf	5,37E-05	6.76E-06	3.30E-02	no
Cobalt •	8.40E-05	lb/10 ⁸ scf	3.22E-06	4.06E-07	3.30E-03	no
Copper	8,50E-04	lb/10 ⁶ scf	3.26E-05	4.11E-06	3.33E-01	no
Dibutylphthalate	FNA	lb/10 ⁶ scf	FNA	FNA	6.70E-02	no
Dichlorobenzene	1.20E-03	lb/10 ⁶ scf	4.60E-05	5.80E-06	2.00E+01	no
Ethylbenzene	FNA	lb/10 ⁶ scf	FNA	FNA	2.90E+01	no
Fluorene	2.80E-06	lb/10 ⁶ scf	1.07E-07	1.35E-08	1.33E-01	no
Formaldehyde	7.50E-02	lb/10 ⁶ scf	2.88E-03	3.62E-04	5.10E-04	yes.
Hexane	1.80E+00	lb/10 ⁵ scf	6.90E-02	8.69E-03	1.20E+01	no
Manganese	3.80E-04	lb/10 ⁸ scf	1.46E-05	1.84E-06	3.33E-01	no
Mercury	2.60E-04	lb/10 ⁶ scf	9.97E-06	1.26E-06	3.00E-03	no
Molybdenum	1.10E-03	lb/10 ⁸ scf	4.22E-05	5.31E-06	3.33E-01	no
Naothalene	6.10E-04	lb/10 ⁶ scf	2.34E-05	2.95E-06	3.33E+00	no
Nickel	2.10E-03	lb/10 ⁶ scf	8.05E-05	1.01E-05	2.70E-05	yes.
Pentane	2.60E+00	lb/10 ⁶ scf	9.97E-02	1.26E-02	1.18E+02	no
Phenol	FNA	lb/10 ⁸ scf	FNA	FNA	1.27E+00	no
Selenium	<2.4E-5	lb/10 ⁶ scf	9.20E-07	1.16E-07	1.30E-02	no
Toluene	3.40E-03	lb/10 ⁶ scf	1.30E-04	1.64E-05	2.50E+01	no
Vanadium	2.30E-03	lb/10 ⁶ scf	8.82E-05	1.11E-05	3.00E-03	no
o-Xylene	FNA	lb/10 ⁶ scf	FNA	FNA	2.90E+01	no
Zinc	2.90E-02	lb/10 ⁶ scf	1,11E-03	1.40E-04	6.67E-01	no

- (a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be limited, rather than the fuel consumption of the individual boilers. Detailed annual emission estimates for the "Boiler Bubble" are presented in a separate spreadsheet.
- (b) Emission Factors from AP-42 Chapter 1.4, "Natural Gas Combustion".
- (c) IDAPA 58.01.01.585 and 586
- (d) IDAPA 58.01.01.210.05(b)
- * FNA Factor Not Available

Annual Air Pollutant Emissions Boiler Bubble

Combustion Source Characteristics

Natural Gas

ing Value (BTU/scf)

1,020

Jal Fuel Consumption (scf/yr)

1,100,000,000

eria Polluta				Potential	Significant	Below	
		Emission	Emission	Emissions	Level ^c	Regulatory	Significant
Pollutant	Pollutant Source	Factor. ^b	Factor Unit	(TPY)	(TPY)	Concern? ^d	Contribution?
PM ₁₀	NG Combustion	7.6	lb/10 ⁶ scf	4.180	15	no	no
SO ₂	NG Combustion	0.6	lb/10 ⁶ scf	0.330	40	yes	no
NO _x	NG Combustion	100	lb/10 ⁶ scf	55.000	40	no	yes
СО	NG Combustion	84	lb/10 ⁶ scf	46.200	100	no	no
voc	NG Combustion	5.5	lb/10 ⁶ scf	3.025	40	yes	no
Lead	NG Combustion	0.0005	lb/10 ⁶ scf	2.75E-04	0.6	yes	no

-Criteria P	ollutants with Signific	ant Thresho	ld			,	
				Potential	Significant	Below	
		Emission	Emission	Emissions	Level ^c	Regulatory	Significant
Pollutant	Poliutant Source	Factor ^b	Factor Unit	(TPY)	(TPY)	Concern?d	Contribution?
PM	NG Combustion & Process	See PM ₁₀	See PM ₁₀	4.180	25	no	no
3eryllium	NG Combustion	<1.2E-5	lb/10 ⁶ scf	6.60E-06	0.0004	yes	no
Mercury	NG Combustion	2.60E-04	lb/10 ⁶ scf	1.43E-04	0,1	yes	no

Pollutant	Pollutant Source	Emission Factor ^b	Emission Factor Unit	Potential Emissions (TPY)
TOC	NG Combustion	11	lb/10 ⁶ scf	6,050
Methane	NG Combustion	2.3	lb/10 ⁶ scf	1.265
CO ₂	NG Combustion	120,000	lb/10 ⁶ scf	66,000
N ₂ O	NG Combustion	2.2	lb/10 ⁶ scf	1.210

o facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual tel consumption of the bubble will be monitored and limited to 1,100,000,000 scf/yr

JAPA 58.01.01.006.92)APA 58.01.01.221.01

Annual Toxic Air Pollutant Emissions Boiler Bubble

Combustion Source Characteristics

Fuel

Natural Gas

Heating Value (BTU/scf)

1,020

Annual Fuel Consumption (scf/yr)*

1,100,000,000

Toxic Air Pollutants			
Pollutant	Emission Factor ^b	Emission Factor Unit	Potential Emissions (TPY)
Arsenic	2.00E-04	lb/10 ⁶ scf	1.10E-04
Barium	4.40E-03	lb/10 ⁶ scf	2.42E-03
Benzene	2.10E-03	lb/10 ⁶ scf	1.16E-03
Beryllium	<1.2E-5	lb/10 ⁶ scf	6.60E-06
Benzo(a)pyrene	<1.2E-6	lb/10 ⁶ scf	6.60E-07
Bis (2-ethylhexyl)phthalate	FNA	lb/10 ⁶ scf	FNA
Cadmium	1.10E-03	lb/10 ⁶ scf	6.05E-04
Chromium	1.40E-03	lb/10 ⁶ scf	7.70E-04
Cobalt	8.40E-05	lb/10 ⁶ scf	4.62E-05
Copper	8.50E-04	lb/10 ⁶ scf	4.68E-04
Dibutyiphthal ate	FNA	lb/10° scf	FNA '
Dichlorobenzene '	1.20E-03	lb/10 ⁶ scf	6.60E-04
Ethylbenzene	FNA	lb/10 ⁶ scf	FNA
Fluorene	2.80E-06	lb/10 ⁶ scf	1.54E-06
Formaldehyde	7.50E-02	lb/10 ⁶ scf	4.13E-02
Hexane	1.80E+00	lb/10 ⁶ scf	9.90E-01
Manganese	3.80E-04	lb/10 ⁶ scf	2.09E-04
Mercury	2,60E-04	lb/10 ⁶ scf	1.43E-04
Molybdenum	1,10E-03	lb/10 ⁶ scf	6.05E-04
Napthalene	6.10E-04	lb/10 ⁶ scf	3.36E-04
Nickel	2.10E-03	lb/10 ⁶ scf	1.16E-03
Pentane	2.60E+00	lb/10 ⁶ scf	1.43E+00
Phenol	FNA	lb/10 ⁶ scf	FNA
Selenium	<2.4E-5	lb/10 ⁶ scf	1.32E-05
Toluene	3.40E-03	/ lb/10 ⁶ scf	1.87E-03
Vanadium	2.30E-03	lb/10 ⁶ scf	1.27E-03
o-Xylene	FNA	lb/10 ⁶ scf	FNA
Zinc	2.90E-02	lb/10 ⁶ scf	1.60E-02

⁽a) To facilitate operational flexibility, the four boilers at the facility are grouped in a bubble. The annual fuel consumption of the bubble will be monitored and limited to 1,100,000,000 scflyr

⁽b) Emission Factors from AP-42 Chapter 1.4, "Natural Gas Combustion".

^{*} FNA - Factor Not Available

Emission Calculations - Batter Room Dust Collector (E209)

Description

Several of the potato products processed at the McCain Foods facility in Burley, Idaho are battered. Batters are prepared from various dry ingredients, such as starch and seasonings, in the Batter Room in the Burley 2 Plant. Particulate matter is filtered from the air in the Batter Room via a dust control system that is manufactured by DCE, Inc. The system consists of a cased group of filter elements and is equipped with its own fan and discharge arrangements.

PM / PM₁₀ Emission Rates

Equipment Data:

Model: Dalamatic Dust Control Unit

Unit Designation Number DU204F6AD

Outlet Emission Rate 0.00437-0.00874 gr/dscf

Fan Designation F6 Fan Size
Fan Air Volume 1,600 dscfm

No. of Filter Elements 20 Envelope Length 39.5"

Dust Container Volume 4 ft³

Calculations:

PM₁₀ Hourly Emission Rate = $(0.00874 \text{ gr/dscf}) \times (1,600 \text{ dscfm}) \times (60 \text{ min/hr})$ (7,000 gr/lb)

PM₁₀ Hourly Emission Rate = 0.120 lb/hr

PM₁₀ Annual Emission Rate = $(0.120 \text{ lb/hr}) \times (8,760 \text{ hr/yr})$ (2000 lb/ton)

PM₁₀ Annual Emission Rate = 0.525 ton/yr

Process Weight Rule Compliance - Exempt

This emission source qualifies for the De Minimis Exception per IDAPA 58.01.01.710.02.

Air Pollutant Emissions Emergency Fire Pump (E001)

Combustion Source Chara	cteristi cs	Stack Data	
ınufacturer	Detroit Diesel	Stack Height (ft)	6.08
del	6061-A2	Stack Diameter (ft)	0.33
wer Output (hp)	170	Exit Gas Temperature (°F)	445.
el	Diesel	Wet Actual Flow Rate (acfm)	289
ated Input (MMBTU/hr)	0.844	Wet Standard Flow Rate (wscfm)	145
eating Value (BTU/lb)	19,300	Dry Standard Flow Rate (dscfm)	129
sauly voice (D10).D/		Stack Velocity (m/s)	16.8
Site Information	<u> </u>	Fd (dscf stack gas/BTU)	0.00919
rrley Barometric Pressure (mm Hg)	654.18	Fw (wscf stack gas/BTU)	0.01032
tual Hours of Operation (hr/Vf)	104		

riteria Pollutai		Emission	Emission	Potential Emissions	Potential Emissions	Potential Emissions	Significant Level ^b	Below Regulatory	Significant Contribution
Pollutant	Pollutant Source	Factor*	Factor Unit	(lb/hr)	(TPY)	(g/s)	(TPY)	Concern? ^c	
PM ₁₀	Diesel Combustion	2.20E-03	lb/hp-hr	0.374	0.019	0.047	15	yes	no
SO ₂ (SO, Basis)	Diesel Combustion	2.05E-03	lb/hp-hr	0.349	0.018	0.044	40	yes	no
NO _x	Diesel Combustion	0.031	lb/hp-hr	5.270	0.274	0.664	40	yes	no
co	Diesel Combustion	6.68E-03	lb/hp-hr	1.136	0.059	0.143	100	yes	no
OC (TOC Basis)	Diesel Combustion	2.51E-03	lb/hp-hr	0.427	0.022	0.054	40	yes	no
Lead	Diesel Combustion	FNA	FNA	FNA	FNA	FNA	0.6	yes	no

on-Criteria Po	ollutants with Signific	cant Thresho	ld						-
▶ Pollutant	Pollutant Source	Emission Factor*	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emissions (g/s)	Significant Level ^b (TPY)	Below Regulatory Concern? ^e	Significant Contribution مو
PM	Diesel Combustion	See PM ₁₀	See PM ₁₀	0.374	0.019	0.047	25	yes	no
Beryllium	Diesel Combustion	FNA	FNA	FNA	FNA	FNA	0.0004	FNA	FNA
Mercury	Diesel Combustion	FNA	FNA	FNA	FNA	FNA	0.1	FNA	FNA

Pollutant	Pollutant Source	Emission Factor*	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (TPY)	Potential Emission: (g/s)
TOC	Diesel Combustion	2.51E-03	lb/hp-hr	0.427	0.022	0.054
Methane	Diesel Combustion	FNA	FNA	FNA	FNA	FNA
CO ₂	Diesel Combustion	1.15	lb/hp-hr	196	10.166	24.633
N ₂ O	Diesel Combustion	FNA	FNA	FNA	FNA	FNA

'M Grain Loading Standard^d Not Applicable

'rocess Weight Rule - Exempt

lotes:

- a) Emission Factors from AP-42 Chapter 3.3, "Gasoline and Diesel Industrial Engines".
- b) IDAPA 58.01.01.006.92
- c) IDAPA 58.01.01.221.01
- d) IDAPA 58.01.01.676 or 677.- The fire pump does not satisfy the definition of "fuel burning equipment" as presented in IDAPA 58.01.01.006.41.
- IDAPA 58.01.01.710.02 This emission source qualifies for the De Minimis Exception FNA Factor Not Available

Toxic Air Pollutant Emissions Emergency Fire Pump (E001)

Combustion Source Characteris	tics	Stack Data	
Manufacturer	Detroit Diesel	Stack Height (ft)	6.08
Model	6061-A2	Stack Diameter (ft)	0.33
Power Output (hp)	170	Exit Gas Temperature (%F)	445
Fuel	Diesel	Wet Actual Flow Rate (acfm)	289
Rated Input (MMBTU/hr)	0.844	Wet Standard Flow Rate (wscfm)	145
Heating Value (BTU/lb)	19,300	Dry Standard Flow Rate (dscfrn)	129
Trooping Talwa (m.)		Stack Velocity (m/s)	16,8
Site Information	•	Fd (dscf stack gas/BTU)	0.00919
Burley Barometric Pressure (mm Hg)	654.18	Fw (wscf stack gas/BTU)	0.01032
Actual Hours of Operation (hr/yr)	104	•	

Pollutant	Emission Factor *	Emission Factor Unit	Potential Emissions (lb/hr)	Potential Emissions (g/s)	Emission Limit ^a (lb/hr)	Modeling Required?
Arsenic	FNA .	FNA	ENA	FNA	1.50E-06	no
Barium	FNA	FNA	FNA	FNA	3.30E-02	no
Benzere	9,33E-04	Ib/MMBTU	7.87E-04	9.92E-05	8.00E-04	no
Beryllium	FNA	FNA	FNA	FNA	2.80E-05	no
Benzo(a)pyrene	1.88E-07	Ib/MMBTU	1.59E-07	2.00E-08	2.00E-06	no
Bis (2-ethylhexyl)phthalate	FNA	FNA	FNA	FNA	2.80E-02	no
Cadmium	FNA	FNA	FNA	FNA	3.70E-06	no
Chromium	FNA	FNA	FNA	FNA	3.30E-02	по
Cobelt	. FNA	FNA	FNA	FNA	3.30E-03	no
Copper	FNA	FNA	FNA	FNA	3.33E-01	no
Dibutylphthelate	FNA	FNA	FNA	FNA	6.70E-02	no
Dichlorobenzene	FNA	FNA	FNA	FNA	2.00E+01	no
Ethylbenzene	FNA	FNA	FNA	FNA	2.90E+01	no
Fluorene	2.92E-05	Ib/MMBTU	2.46E-05	3.11E-06	1.33E-01	no
Formaldehyde	1.18E-03	Ib/MMBTU	9.96E-04	1.25E-04	5.10E-04	yes
Hexane	FNA	FNA	FNA	FNA	1.20E+01	no
Manganese	FNA	FNA	FNA	FNA	3.33E-01	no
Mercury	FNA	FNA	FNA	FNA	3.00E-03	l no
Molybdenum	FNA	FNA	FNA	FNA	3.33E-01	no
Napihalene	8.48E-05	Ib/MMBTU	7.16E-05	9.02E-06	3.33E+00	no
Nickei	FNA	FNA	FNA	FNA	2.70E-05	l no
Pentane	FNA	FNA	FNA	FNA	1.18E+02	no
Phenol	FNA	FNA	FNA	FNA	1.27E+00	no
Selenium	FNA	FNA	FNA	FNA	1.30E-02	no
Toluene	4.09E-04	Ib/MMBTU	3,45 E-04	4.35E-05	2.50E+01	· no
Vanadium	FNA	FNA	FNA	FNA	3.00E-03	
	2.85E-04	Ib/MMBTU	2.41E-04	3.03E-05	T	l no
o-Xylene (Based on Xylenes) Zinc	2.60E-04 FNA	FNA	2,41E-04 FNA	3,03E-05 FNA	2.90E+01 6.67E-01	no no

- (a) Emission Factors from AP-42 Chapter 3.3, "Gasoline and Diesel Industrial Engines".
- (b) IDAPA 58,01.01.585 and 586
- (c) IDAPA 58.01.01.210.05(b)
- FNA Factor Not Available

combination with other contaminants, injure or unreasonably affect human or animal life or vegetation." To demonstrate compliance with this requirement, an inventory of all TAP emissions at the facility was performed. IDAPA 58.01.01.585 and 586 provide a list of compounds that are considered TAPs. The list also provides screening emission levels and acceptable ambient concentrations that are used for evaluating proposed newsources. The following is a description of DEQ's method for evaluating compliance with IDAPA 58.01.01.161 with regard to this Facility wide Tier II OP application:

- Inventory all TAP emissions at the facility. The lb/hr value associated with maximum 24-hour averaged emissions is used for non-carcinogenic TAPs listed in IDAPA 58.01.01.585, and the Ib/hr value associated with maximum annual averaged emissions is used for carcinogenic TAPs listed in IDAPA 58.01.01.586.
- Compare facility-wide TAP emissions with screening emission levels provided in IDAPA 58.01.01.585 and 586. If emissions are less than screening levels, then no further analyses are required.
- 3) Non-carcinogenic TAPs with emissions that exceed the screening levels must be modeled to evaluate the maximum 24-hour impact to ambient air. If maximum impacts are less than the applicable acceptable ambient concentration (AAC), then no further analyses are required. If maximum impacts are greater than AACs, approval will be evaluated on a case-by-case basis, considering:
 - uncertainty of emission factors and human health impact data,
 - magnitude and frequency of modeled impacts exceeding the AAC,
 - public access to the area(s) where modeled impacts exceed the AAC,
 - specific toxicological factors of the TAP.
- 4) Carcinogenic TAPs with emissions that exceed the screening levels must be modeled to evaluate the maximum annual impact to ambient air. The individual cancer risk associated with the maximum long-term modeled concentration will be calculated from the Unit Risk Factor (URF), given in IDAPA 58.01.01.586, for each carcinogenic TAP emission that exceeds the screening level. Impacts are considered acceptable if the maximum cumulative risk (calculated by summing the risk of all modeled carcinogenic TAPs) is less than 1.0 E-5 (1 in 100,000).

Table 1. Applicable Regulatory Limits

Pollutant	Averaging Period	Regulatory Limit ^a (μg/m ³) ^b	Modeled Value Used ^e
Oxides of nitrogen	Annual	100"	1 st highest
Sulfur dioxide	3-hour	1,300	2 nd highest
	24-hour	· 365	2 ^{re} highest
	Annual	80°	1* highest
Carbon monoxide	1-hour	40,000	2 nd highest
	8-hour	10,000	2 ^{to} highest
PM ₁₀	. 24-hour	150'	6" highest
* *****	Annual	50°	1 st highest

^{*} IDAPA 58.01.01.577

b Micrograms per cubic meter

When using five years of meteorological data

^d Particulate matter with an aerodynamic diameter less than or equal to a nominal 10 micrometers

^{*} Not to be exceeded

¹ Not to be exceeded more than once per year

2.3 Background Concentrations

DEQ provided McCain Foods with appropriate background concentrations for use in the Tier II OP application. Background PM₀ concentrations were obtained from monitoring data collected in Rupert, Idaho. Statewide background concentrations were used for all other criteria pollutants. Table 2 lists applicable background concentrations.

Table 2. Background Concentrations

Pollutant	Averaging Period	Background Concentration (μg/m³)*
Oxides of nitrogen (NO _x)	Annual	40
Sulfur dioxide (SO ₂)	3-hour	374
	24-hour	120
	Annual	- 18.3
Carbon monoxide (CO)	1-hour	11,450
	8-hour	5,130
PM ₁₀ °	24-hour	. 100
* ************************************	Annual	25.1

Micrograms per cubic meter

2.4 Modeling Impact Assessment

Ambient impact analyses were performed by McCain Foods' consultant, Mllennium Science & Engineering, Inc. (MSE), using the model ISCST3 - VERSION 00101. A modeling protocol was submitted to and approved by DEQ prior to submittal of the Tier II OP application. Table 3 provides a summary of modeling parameters used.

Table 3. Modeling Parameters

Parame ter	Description/Values	Documentation/Additional Description
Model	ISCST3	Version 0010
Meteorological Data	Pocatello, idaho (surface) Boise, idaho (upper air)	1987-1991
Model Options	Regulatory Default	
Land Use	Rural	
Terrain	Simple	Approved by DEQ provided maximum impacts are near the facility property boundary
Building Downwash	Used BPIP program and building dimensions	See Figure 1 and 2 for building, source, and receptor locations
Receptor grids See Figure 1	Grid 1	30 meter spacing along site boundary out to 90 meters
	Grid 2	100 meter spacing out to about 300 meters from the east-most boundary point, 500 meters from the southern and western boundary, 800 meters from the north-most boundary point

Meteorological data were not available for the Burley area. Therefore, Pocatello surface data were used in combination with Boise upper air data. Use of these data did not enable consideration of local meteorological effects induced by the presence of the Snake River. This limitation did not likely result in a substantial change in the results of the analyses.

DEQ checked the ISCST3 meteorological input fle used by the applicant against DEQ generated meteorological fles. For five years of hourly data, differences between the files were found for eight hours of data. Although the differences would not likely result in any change in the modeling results, DEQ verification modeling was performed using meteorological fles consistent with DEQ generated data.

Particulate matter with an aerodynamic diameter less than or equal to a nominal 10 micrometers

DEQ performed verification modeling, using ISCST3 – Version 02035, to check the results submitted by the applicant. Differences between results for the two versions of ISCST3 were negligible.

Table 4 provides a summary of emission rates used in the criteria pollutant modeling analyses and Table 5 provides a summary of emission rates used in the TAP modeling analyses. Compliance with annual air quality standards was conservatively based on using maximum hourly emission rates rather than maximum annual emission rates. Ambient impacts from allowable annual emissions would be less than those indicated fom using maximum hourly rates. McCain Foods also requested an annual emission bubble for the boilers (a single emission limit for the combination of the four boilers). However, the annual ambient impacts were based on the maximum hourly emission rates from each boiler, assuming each boiler operates continuously throughout the year. This approach results in the use ofemission rates for modeling that are considerably greater than permitted allowable rates. Consequently, the actual ambient impacts will likely be less than those predicted bythe atmospheric dispersion modeling.

Table 4. Pollutant Emission Rates Used for Criteria Pollutant Modeling

Source (ld Code)	Maximum Hourly Emission Rate ^a (lb/hr) ^c				Hourly Rate use for Annual Modeling ^b (lb/hr)			
Pollutant	PM ₁₀ [©]	SO ₂ *	NO _x	COs	PM ₁₀	SO ₂	NO _x	CO
Party Fryer Air Washer (F108)	1.30	NA	NM'	NA	1,30	NA	NA .	NM
Tot Fryer Air Washer (F103)	4,08	NA	NM ¹	NA	4.08	NA.	NA	NM
Prime 1 Fryer Air Washer (F104)	2.68	NA	NM ¹	NA	2.68	NA	NA	NM'
Prime 2 Fryer Air Washer (F204)	2.25	NA	NM	NA	2,25	NA	NA.	NM
Tot Dryet (D107)	2.00	0.00235	NM ¹	1.46	2.00	0.00235	0.603	NM
Prime 1 Dryer (D105 and D106)h	3.35	0.00397	NM ¹	2.56	3.35	0.00397	1.05	NM
Prime 2 Dryer (D205 – D208)*	1.41	0.00794	NM	4.39	1.41	0.00794	1.80	NM
Murray 1 Boiler (B101)	0.75	0.0556	NM'	8.24	0.75	0.0556	9.80	NM
Murray 2 Boiler (B203)	0.29	0.0238	NM ¹	3,22	0.29	0.0238	3.83	NM
Nebraska 1 Boiler (B102)	0.71	0.0556	NM	7.87	0.71	0.0556	9.37	NM'
Nebraska 2 Boiler (B202)	0.58	0.0476	NM ¹	6.43	0.58	0:0478	7.85	NM
Batter Room Dust Collector (E209)	0.12	NA	NM'	NA	0.12	NA	NA	· NM
Emergency Fire Pump (E001)	0.37	0.349	NM	1.14	0.37	0.349	5.27	NM

^{*}Emission rate used for 24-, 8-, 3-, and 1-hour averaging periods

Table 5. Pollutant Emission Rates Used for TAP Modeling

Source (Id Code)	Hourly Rate use for Modeling (lb/hr)*								
Pollutant	Hydrogen Sulfide ^b	Arsenic ^e	Benzene ^c	Cadmium ^e	Formal- dehyde ^s	Nickel			
Party Fryer Air Washer (F108)	NA NA	NA	NA NA	NA NA	NA	NA.			
Tol Fryer Air Washer (F103)	NA NA	NA	NA	NA NA	NA	NA			
Prime 1 Fryer Air Washer (F104)	NA NA	NA	NA	NA	NA	NA.			
Prime 2 Fryer Air Washer (F204)	NA NA	NA	NA	NA NA	NA	NA			
Tot Dryer (D107)	NA NA	7.84E-7	8,25E-6	4.32E-6	2.94E-4	8,25E-6			
Prime 1 Dryer (D105 and D106)*	NA NA	1.37E-6	1.44E-5	1,54E-5	5,16E-4	1.44E-5			
Prime 2 Dryer (D205 - D206) ^d	NA NA	2.36E-6	2.48E-5	1.29E-5	8.83E-4	2.48E-5			
Murray 1 Boiler (B101)	NA NA	1.96E-5	2.06E-4	1.08E-4	7.35E-3	2.06E-4			
Murray 2 Boilet (B203)	NA NA	7.67E-6	8.02E-5	4.21E-5	2.87E-3	8.02E-5			

^b Emission rate used for annual averaging period

Pounds per hour

^{*}Particulate matter with an aerodynamic diameter less than or equal to a nominal 10 micrometers

^{*}Sulfur dioxide

Oxides of nitrogen

Carbon monoxide

h Emissions rate per each unit

Not modeled because there is no applicable standard for the specified averaging time

Table 5. Pollutant Emission Rates Used for TAP Modeling

Source (Id Code)	Hourly Rate use for Modeling (lb/hr) ^a							
Pollutant	Hydrogen Sulfide ^b	Arsenic	Benzene ^c	Cadmium ^e	Formal- dehyde ^e	Nickel ⁶		
Nebraska 1 Boiler (B102)	NA	1.87E-5	1.97E-4	1.03E-4	7.03E-3	1.97E-4		
Nebraska 2 Boiler (8202)	NA	1.53E-5	1.60E-4	8.41E-5	5.74E-3	1.60E-4		
Batter Room Dust Collector (E209)	-NA	NA NA	NA	NA NA	NA .	NA		
Emergency Fire Pump (E001)	NA	NA NA	7.87E-4	NA	9.92E-4	NA		
Anaerobic Treatment Basin (A100)	4.83	NA	NA.	NA NA	NA	NA		

Pounds per hour

d Emissions rate per each unit

Table 6 lists the emission release parameters used in the dispersion modeling analyses and Figure 2 shows building and emission point locations. All emissions are released to the atmosphere through stacks except for the Anaerobic Treatment Basin. This source was modeled as a 210-foot by 361-foot ground-level area source. Emissions from the Batter Room Dust Collector and the Emergency Fire Pump vent horizontally through a wall vent. The stack diameter and stack gas flow velocity associated with these sources were modeled with values of 0.001 meters and 0.001 meters per second, respectively, to prevent improper consideration of stack tip downwash and momentum plume rise.

Table 6. Emission and Stack Parameters

Source / Location	Source Type	Stack Height (m)*	Stack Dis. (m)	Stack Gas Temp. (K) ⁶	Stack Gas Flow Velocity (m/sec) ^c
Party Fryer Air Washer (F108)	Point	16.0	0.95	311	7.20
Tot Fryer Air Washer (F103)	Point	16.35	1.13	328	8.13
Prime 1 Fryer Air Washer (F104)	Point	18.0	0.95	353	8.91
Prime 2 Fryer Air Washer (F204)	Point	13.6	0.97	342	13.38
Tot Dryer (D107)	Point -	16.0	0.91	321	13.92
Prime 1 Dryer - Stack East (D105)	Point	18,5	1.03	375	9.27
Prime 1 Dryer - Stack West (D106)	Point	18.5	1.03	344	8.19
Prime 2 Dryer – Stack #1 (D205)	Point	12.0	1.46	318	11.38
Prime 2 Dryer - Stack #2 (D206)	Point	12.0	1.46	314	12.16
Prime 2 Dryer - Stack #3 (D207)	Point	12.0	1.46	319	10.12
Prime 2 Dryer - Stack #4 (D208)	Point	12.0	1.46	309	11.34
Murray 1 Boiler (B101)	Point	12.41	1.52	426	7,73
Murray 2 Boiler (B203)	Point	11.56	0.91	426	8.39
Nebraska 1 Boiler (B102)	Point	19.79	1.22	426	11.54
Nebraska 2 Boiler (B202)	Point	20.38	0.91	426	16.76
Better Room Dust Collector (E209)	Point	2.64	0.001	0	0.001
Emergency Fire Pump (E001)	Point	1.85	0.001	502.59	0.001
Anaerobic Treatment Basin (A100)	Area	NA	NA	NA	NA

Meters

Lead (Pb) was not included in the dispersion modeling analyses. Potential Facility-wide Pb emissions were estimated at 3.31 E-4 tons per year (TPY). This emission level is over three orders of magnitude less than the significant emission level (IDAPA 58.01.01.006. 92) and two orders of magnitude less than the value defined as "below regulatory concern" for permit to construct (PTC) applicability (IDAPA 58.01.01.221.01). Therefore, it was concluded that Pb emissions from the facility could not reasonably be expected to cause or significantly contribute to a violation of the Pb NAAQS.

Non-carcinogen, emission rate used for modeling the maximum 24-hour average

^c Carcinogen, emission rate used for modeling the maximum annual average

b Kelvin

^c Meters per second

A significant impact analysis was initially performed to determine if emissions resulting from operation of the facility would "significantly contribute" to pollutant concentrations in arbient air. A full impact analysis was then performed for those pollutants emitted from the facility that were estimated to have an ambient impact exceeding "Significant Contribution" levels. The full impact analysis involved adding the dispersion modeling results to background concentrations.

3. MODELING RESULTS:

Modeled ambient air impact results from the significant impact analysis are provided in Table 7. Because the impact from facility emissions exceeded significant contribution levels for annual NO_2 , annual PM_{10} , 24-hour PM_{10} , 24-hour SO_2 , 3-hour SO_2 , and 1-hour CO, a full impact analysis was performed for those pollutants and averaging times.

Nitrogen dioxide concentrations were conservatively estimated by assuming 100% of NOx is NO₂. Results of the full impact analysis are presented in Table 8, and indicate that operation of the facility as described in the Tier II OP application will not cause or significantly contribute to a violation of a NAAQS. Modeled PM₁₀ impacts of 144 µg/m³ (including background) are approaching the 24-hour NAAQS of 150 µg/m³. However, this concentration level is confined to a relatively small area along the facility's northern boundary, as shown in Figure 3. The predominant north/south concentration contours may be a result of using surface meteorological data from Pocatello. The presence of the Snake River near the site would be expected to cause concentration contours with a more predominant east/west component.

Table 7. Significant Impact Analysis for Criteria Pollutants.

Pollutant	Averaging Period	Ambient Concentration (µg/m³)*	Significant Contribution ^b (µg/m³)	Full Impact Analysis Required (Y or N)
Nitrogen dioxide (NO ₂)	Annual	12.4°	1.0	Y
Sulfur dioxide (SO ₂)	3-hour	187*	25	Y
	24-hour	29	5	Y
1	Annual	0.32	1.0	N
Carbon monoxide (CO)	1-hour	2,575	2,000	Ÿ
	8-hour	323	500	· N
PM ₁₀ ⁵	24-hour	44'	5.0	Υ
	Annual	10.4°	1.0	Υ

Micrograms per cubic meter

Table 8. Full Impact Analysis for Criteria Pollutants.

Pollutant	Averaging Period	Ambient Concentration (μg/m³)*	Background Concentration (µg/m³)	Total Ambient Concentration (μg/m³)	Regulatory Limit ^b (μg/m ³)	Compliant (Y or N)
Nitrogen dioxide (NO ₂)	Ann ual	12.4°	40.0	52	100	Y
Sulfur	3-hour	187*	374	561	1,300	Y
dioxide (SO ₂)	24-hour	29*	120	149	365	Y

b Significant Contribution level as per IDAPA 58.01.01.006.93.

^{*}Particulate matter with an aerodynamic diameter less than or equal to a nominal 10 micrometers

First highest modeled value

^{*} Second highest modeled value

Sixth highest modeled value

Table 8. Full Impact Analysis for Criteria Pollutants.

Pollutant	Averaging Period	Ambient Concentration (µg/m³)*	Background Concentration (µg/m³)	Total Ambient Concentration (µg/m³)	Regulatory Limit ^b (μg/m³)	Compliant (Y or N)
Carbon monoxide (CO)	1-hour	2,575*	11,450	14,025	40,000	Y -
(CO) PM ₁₀ °	24-hour	44'	100	144	150	Y
	Annuel	10.4°	25.1	35.5	50	Y

Micrograms per cubic meter

Potential emissions of non-carcinogenic TAPs were all below screening emission levels, except for hydrogen sulfide (H₂S). Hydrogen sulfide is only emitted from the Anaerobic Treatment Basin. Emissions of H₂S were modeled to predict the maximum 24-hour averaged concentration. Modeled concentrations exceeded the AAC in one area north of the facility along the property boundary. The model was rerun after adjusting artificially low mixing heights to a height of 30 meters, and resulting concentrations still exceeded the AAC. Figure 4 shows maximum modeled H₂S concentration contours for the 24-hour averaging period. Review of the meteorological data associated with dates exhibiting high H₂S concentrations indicated that the high concentrations were a result of very low wind speeds and the close proximity of the emission source to the property boundary. During low winds, the ground level emissions do not significantly disperse before impacting a ground level receptor along the property boundary.

DEQ determined that the modeled 24-hour H₂S impact was acceptable because of the following:

- 1) The area where model results predict an exceedance of the AAC is located between the facility property boundary and the Snake River. Although this area is considered ambient air, there is a very low probability that members of the public could be present during periods when concentrations may exceed the AAC. Furthermore, it is unlikely that any member of the public present at that location and time would remain for a 24-hour period, and therebybe exposed to a 24-hour averaged concentration that exceeds the AAC.
- 2) The maximum modeled concentration was 862 μg/m³, compared to an AAC of 700 μg/m³. This concentration is still well below all occupational exposure limits.
- 3) Over a modeled period of five years, concentrations potentially exceeding the AAC were predicted to occur during only five days (0.3% of the time).

Potential odor concerns were also evaluated by using the maximum measured H₂S emission rate along with hourly averaging periods. Figures 5 and 6 showmaximum 1-hour modeled concentrations. Concentrations may exceed the 11 µg/m³ odor threshold at distances of several kilometers from the property boundary. For comparative purposes, maximum hourly concentrations were well below the NIOSH 10-minute ceiling value of 15,000 µg/m³.

Screening Emission Levels for carcinogenic TAPs were exceeded for arsenic (As), benzene (C₆H₆), cadmium (Cd), formaldehyde (CH₂O), and nickel (Ni). Emissions of these pollutants were then modeled to predict the maximum annual averaged impact and the individual cancer risk associated with exposure to the maximum annual averaged concentration. Table 9 summarizes the carcinogenic TAP analysis. DEQ determined that impacts were acceptable because the maximum total individual cancer risk, associated with exposure to maximum concentrations of all carcinogenic TAPs with emissions exceeding the Screening Emission Levels, was below 1.0 E-5 (1 in100,000).

DAPA 58.01.01.577

^{*}Particulate matter with an aerodynamic diameter less than or equal to a nominal 10 micrometers

d First highest modeled value

^{*}Second highest modeled value

Sixth highest modeled value

Table 9. Carcinogenic TAP Modeling Analysis

Carcinogenic TAP	Maximum Modeled Annual Conc. (μg/m³)	Unit Risk Factor (cancer risk /μg/m³ - person)	Estimated Risk (cancer risk / person)
Arsenic (As)	2 E-5	4.3 E-3	8.6 E-8
Benzene (C ₆ H ₆)	6.2 E-4	8.3 E-6	5.1 E-9
Cadmium (Cd)	1.1 E-4	1.8 E-3	1.98 E-7
Formaldehyde (CH ₂ O)	7.2 E-3	1.3 E-5	9.4 E-8
Nickel (Ni)	2.0 E-4	2.4 E-4	4.8 E-8
		Total Risk	4.3 E-7

The TAPs assessment performed for operations at McCain Foods demonstrated compliance with IDAPA 58.01.01.161 to the satisfaction of DEQ.

Electronic copies of the modeling analysis are saved on disk. Table 10 provides a summary of the files used in the modeling analysis. Stephen Coe has reviewed this modeling memo to ensure consistency with the permit and technical memorandum.

Table 10. Dispersion Modeling Files

Table 10. Dis	persion Modeling Files			
Type of File	Description	File Name		
Met Data	1987-1991 consistent with DEQ date	ModBoiPoc87.txt; ModBoiPoc88.txt; ModBoiPoc89.txt; ModBoiPoc90.txt; ModBoiPoc91.txt;		
BEEST Input	PM ₁₀ 24-hour	PM24hr.BST		
Files	SO224hr.BST			
	CO 8-hour and 1-hour	CO24hr.BST		
•	NO _x annual for each of 5 years			
	PM ₁₀ annual for each of 5 years	PMYY.BST (YY = year 87 - 91)		
	SO ₂ annual for each of 5 years	SO2YY.BST (YY = year 87 - 9	1)	
,	H ₂ S 24-hour	H2S.BST		
	H ₂ S using max emission 1-hour and 24-hour	H2SMex.BST		
	Arsenic period average	As.BST		
	Benzene period average	benzene.BST		
	Cadmium period average	cadmium.BST		
	Formaldehyde period average	formaldehyde.BST		
Nickel nickel,BST				
	as the following type of files associ	ated with it:		
	file for BPIP program		.PIP	
	output file		.TAB	
	ise BPIP output file		.SUM	
	Line file containing direction specif	ic build ing dimensions	.so	
ISCST3 input file .DTA				
ISCS		.LST		
User summary output file			.USF	
Master graphics output file			.GRF	
Some modeling	files have the following type of gra	phics files associated with them		
Surfer data file			.DAT	
Surfer boundary file			.BLN	
Surfer post file containing source locations			.TXT	
Surfe	r plot file		.SRF	
Additional files				
Maps	McCain3.TIF; McCain4.TIF	Background USGS ma	aps	

Receptor, Building, and Source Locations

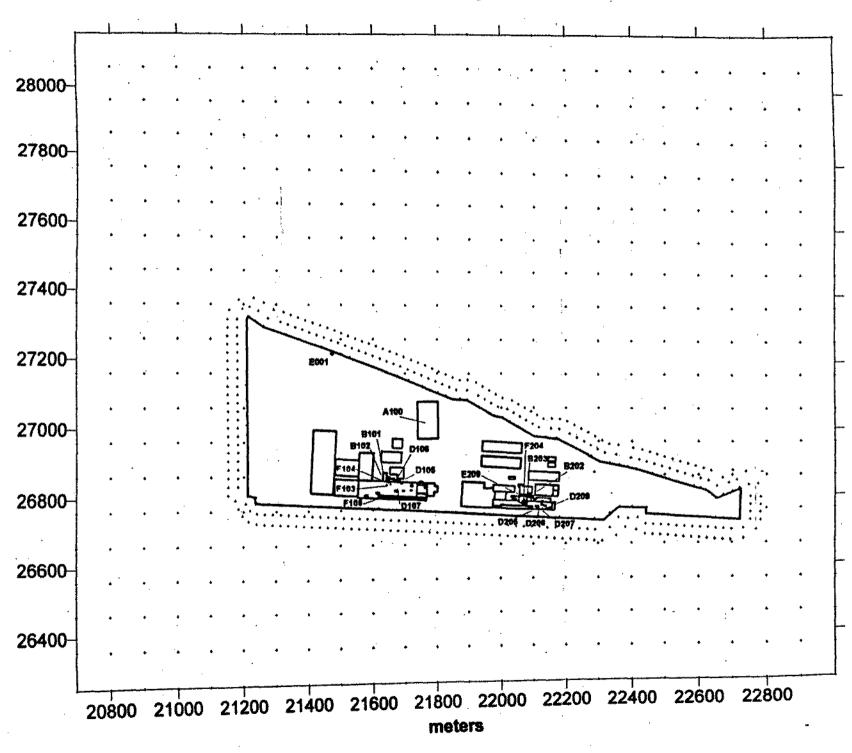
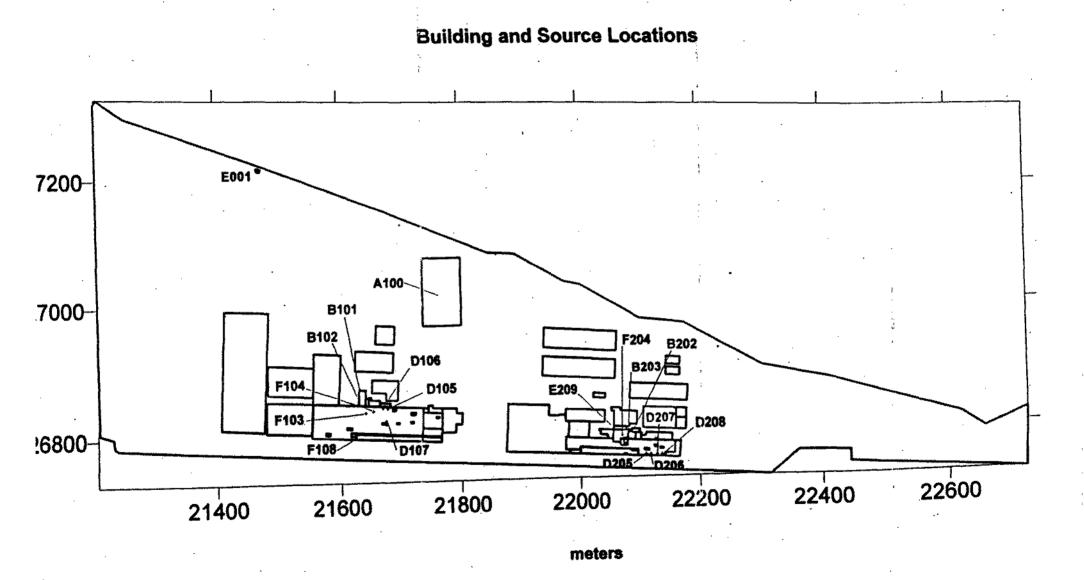
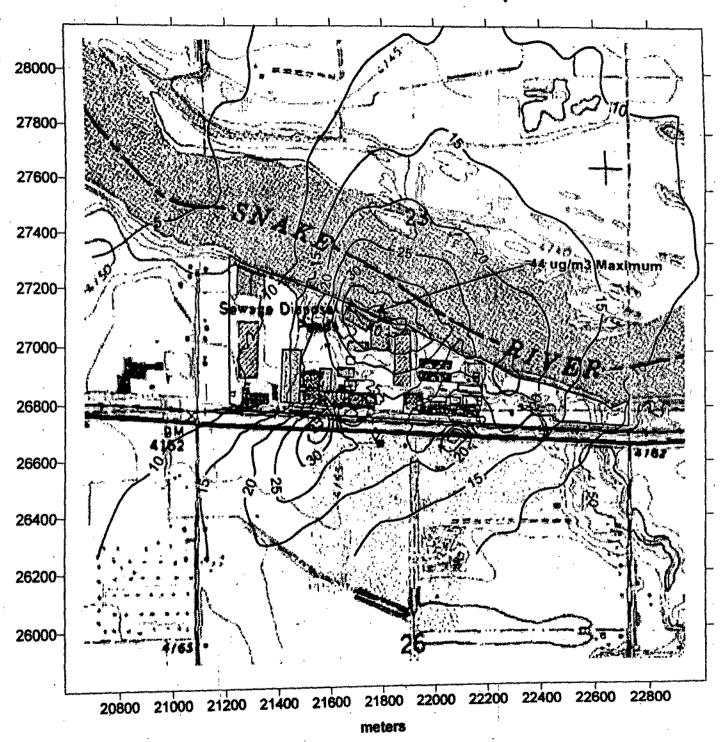


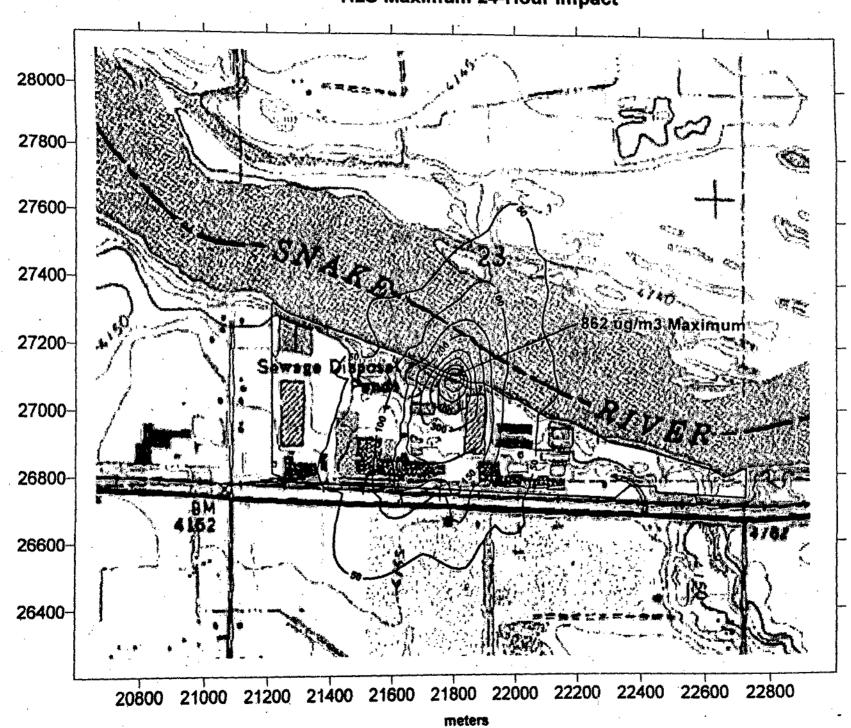
Figure 2 - McCain Foods Tier II Ambient Air Assessment



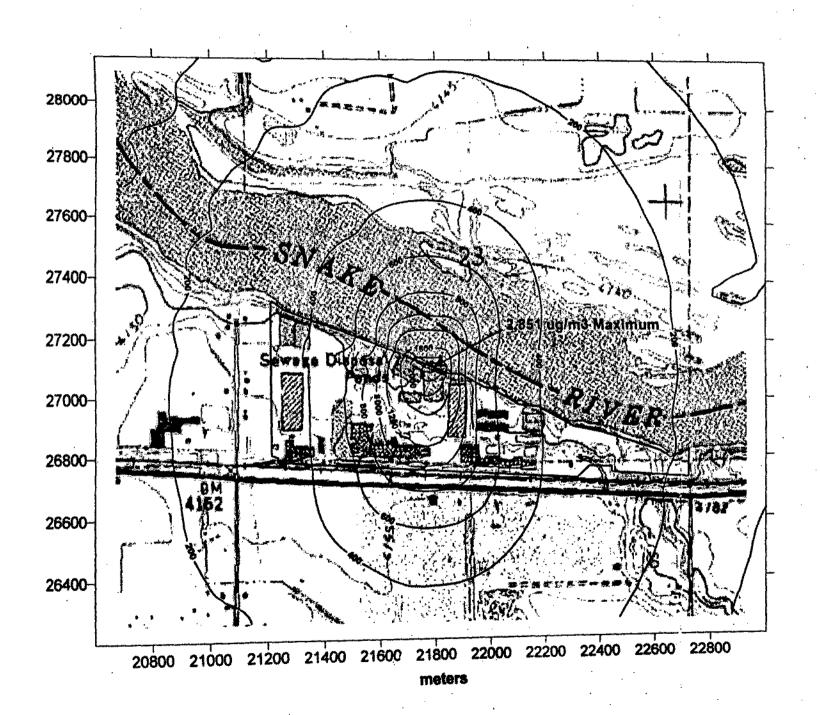
PM-10 Maximum 24-Hour Impact



H2S Maximum 24-Hour Impact



H2S Maximum 1-Hour Impact



Note: 11 ug/m3 odor threshold

ERPG(1) =140 ug/m3

ERPG(2) = 42,000 ug/m: